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An Investigation of Electrodeposited Alloys and Pure Metals as Substitutes for Zinc and Cadpium foz! Protective Finishes for Steel Parts of Aircraft Snavely, C. A.; Tripler, A. B.; Faust, C. L.

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Data are presented on static and dynamic potentials of selected pure metals and alloys relative to SAE-4130 steel, to serve as the basis for selecting the prospective substitutes for pure zinc and cadmium plate. Satisfactory projection of steel in the tropics would require metallic coatings which are inherently more stable than pure zinc and pure dadmium as represented in commercial electroplates on steel. Pure metals such as manganese and aluminum would increase the electrochemical stability without significantly decreasing galvanic protection. Little or no effect on the corrosion resistance of zinc was observed with minor additions of various metals, with the exception of copper, which did make zinc more resistant. Cadmium-zinc alloys were found superior to either zinc or cadmium.

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AN INVESTIGATION OF ELECTRODEPOSITED ALLOYS AND PURE METALS AS SUBSTITUTES FOR ZINC AND CADMIUM FOR PROTECTIVE FINISHES FOR STEEL PARTS OF AIRCRAFT

UNITED STATES AIR FORCE
AIR MATERIEL COMMAND
Wright-Patterson Air Force Base
Dayton, Ohio

Date: 27 April 1948

UNITED STATES AIR FORCE AIR MATERIEL COMMAND WRIGHT-PATTERSON AIR FORCE BASE DAYTON, OHIO

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AN INVESTIGATION OF ELECTRODEPOSITED ALLOYS AND PURE METALS AS SUBSTITUTES FOR ZINC AND CADMIUM FOR PROTECTIVE FINISHES FOR STEEL PARTS OF AIRCRAFT

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FINAL REPORT

on

AN INVESTIGATION OF ELECTRODEPOSITED ALLOYS AND PURE METALS AS SUBSTITUTES FOR ZINC AND CADMIUM FOR PROTECTIVE FINISHES FOR STEEL PARTS OF AIRCRAFT

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ARMY AIR FORCES MATERIALS LABORATORY WRIGHT FIELD, OHIO

from

BATTELLE MEMORIAL INSTITUTE

by

C. A. Snavely, A. B. Tripler, Jr., and C. L. Faust November 30, 1947

AUTHORITY FOR PROJECT

This is the Final Report on the project being conducted under U. S. Government Contract W-33-038-ac-15723 (16940) dated October 23, 1946.

Objective for This Report

The ultimate objective is to define electrodeposited coatings, which, in substitution for zinc and cadmium plate on aircraft steel parts, will provide better protection, particularly in tropical regions.

The immediate objective of the present contract was to provide data on static and dynamic potentials of selected pure metals and alloys relative to S.A.E. X-4130 steel, to serve as the basis for selecting the prospective substitutes for pure zinc and cadmium plate.

INTRODUCTION

Examination of aircraft materiel during and after service and storage in tropical regions revealed that zinc and cadmium plate did not give satisfactory protection to steel parts. Study of the corrosion data and environment showed that moisture condensate from the very humid atmosphere, and salt-containing dusts near the sea shore, considerably decreased the efficacy of galvanic (or sacrificial) protection known for zinc and cadmium on steel exposed in temperate climates.

It was concluded that satisfactory protection of steel in the tropics would require metallic coatings, which offer sacrificial protection, but which are inherently more stable than pure zinc and pure cadmium as represented in commercial electroplates on steel. Evidence pointed toward alloys of zinc and cadmium with metals that would increase the electrochemical stability without significantly decreasing galvanic protection, and toward less noble, pure metals such as manganese and aluminum.

Those alloys having prospects for meeting the requirements would have electrode petentials appreciably more negative than steel in corroding media. First segregation would be revealed by measurement of static electrode potentials and, further, by measurement of dynamic potentials of the substitute metal or alloy in electrical contact with SAE X-4130 when both were submerged in corroding media.

For corroding media in this laboratory survey, the following were selected: 3 per cent sodium chloride solution, distilled water, and distilled water saturated with carbon dioxide.

The results of the potential measurements study would indicate those substitutes most likely to succeed. Any coatings selected as prospective substitutes would need further evaluation under conditions simulating the cyclic condensation of moisture on and drying of the parts in the tropics. Substitute coatings selected on the basis of all tests would be evaluated in field tests, and commercial plating methods would be developed for those finally making the grade.

The successful substitute coating will retain or exceed the large potential difference between zinc and steel (be appreciably less noble than, and, therefore, protective to steel), yet through polarization or passivation effects, the corrosion current will be considerably less than that exhibited by a zinc-steel couple. Consequently, loss of coating will be slower in sacrificial protection. Corrosion products should be as little hygroscopic as possible.

Alloys, which are very near steel in electrode potential or have more noble values, cannot be expected to protect other than because of "envelope" coverage similar to that of nonmetallic coatings.

RESULTS ACCOMPLISHED

The following binary alloys have electrode potentials indicative of prospects for better protection of steel than zinc or cadmium provider:

Alloy System	Range
Zinc - copper	8 - 28 per cent copper
Cadmium - zinc	3 - 90 per cent cadmium
Zinc - silver	4 - 25 per cent silver
Cadmium - silver	3 - 8 per cent silver
Zine - tin	25 - 90 per cent tin
1	

Alloy System

Range

Zinc - nickel

10 - 12 per cent nickel

Zinc - chromium

2 - 5 per cent chromium

Zinc - manganese

3 - 5 per cent manganese

The preparation of alloys and measurement of electrode potentials required a major portion of the efforts on this project. In all, 81 alloys, representing 14 binary systems (as shown below), were investigated:

Alloy System

Composition Range

Zinc - copper

0 - 28 per cent copper

Cadmium - zinc

Complete

Zinc - silver

0 - 44 per cent silver

Cadmium - silver

0 - 32 per cent silver

Zinc - indium

0 - 40 per cent indium

Cadmium - indium

0 - 40 per cent indium

Zinc - tin

Complete

Cadmium - tin

Complete

Zinc - nickel

0 - 47 per cent nickel

Cadmium - nickel

0 - 3 per cent nickel

Zinc - lead

0 - 1 per cent lead and 99 per cent lead

Cadmium - lead

0 - 13 per cent lead

Zinc - chromium

0 - 5 per cent chromium

Zinc - manganese

0 - 10 per cent manganese

Static potentials of all were measured in 3 per cent sodium chloride solution, in distilled water, and in distilled water saturated with carbon dioxide. Dynamic potentials and corrosion currents were measured for all when electrically connected to SAE X-4130 steel in 3 per cent sodium chloride solution. These measurements were made at 90°F. for first examination, and the data are reported herein. Values of electrode potentials at higher and lower temperature are to be made after indication of prospective alloys is complete at 90°F.

Preliminary experiments revealed that solid, cast alloys could be used for this first work in place of electrodeposited alloys. Considerable timesaving resulted because electrodeposition methods were not known for all compositions of alloys studied. Electrodeposition methods will be needed only for those metals or alloys of ultimate selection. Commercial and/or laboratory methods are known for codeposition of metals in the first six alloy systems of the eight showing the most promise at this stage. Further study of plating details remains to be undertaken, in accordance with the findings of the present and subsequent work in continuation of this project.

Relative potential measurements cannot alone completely evaluate the improvement prospects of substitute coatings. For this reason, an accelerated, simulated tropical atmosphere test was developed. Preliminary results with this test indicate that it can further segregate the alloys in regard to performance under tropical conditions. The procedure, a "vet-dry program cycle" was developed in the latter part of the project period, so that cycluation of alloys, selected on the basis of electrode potential measurements, is not yet complete.

Such data as are available show a correlation between alloy composition and resistance to "wet-dry program exposure" for cadmium - zinc and zinc - nickel alloys. Resistance was superior to that of pure zinc as cast metal. Plated costings of cadmium - zinc and zinc - nickel alloys on SAE X-4130 steel have not yet been evaluated, nor have representatives of the other preferred systems been tested to date.

Examination of aircraft parts, after exposure in the tropics, revealed that improved performance for zinc and cadmium plate results from passivation in chromate solutions. The protective film was superficial and subject to destruction by abrasion. Such a passivation throughout the zinc (or cadmium) could, conceivably, provide the degree of improvement being sought. A method is known for electrodepositing zinc appearing solid throughout, but actually containing microscopic porosity. An attempt to passivate and "fill" such a zinc plate "internally" by capillary action to "soak up" chromating solution was not successful in producing a more resistant zinc plate.

It is to be noted that tin is a metal among those showing beneficial alloying effects. Although tin may become a "strategic" metal, its inclusion affords completeness in the testing program. Knowledge of benefits from using tin could be valuable in case of extreme need for critical applications. Two compositions of zinc - lead alloys were produced, containing 13.3 and 17.7 per cent lead, by electrodeposition.

Each had essentially the same static potential as pure zinc in 3 per cent sodium chloride solution. These two alloys might show improvement over pure zinc in corrosion protection. Before they can be included in the list of good prospects, data will be needed on dynamic electrode potentials in couple with bare steel and in "wet-dry program exposure".

A part of this project related to a literature survey, the results of which are summarized herein. Pertinent references are appended in the Bibliography.

SUMMARY OF ESSENTIAL DATA

Literature Survey

An extensive literature survey was conducted prior to the commencement of experimental work. While knowledge concerning tropical corrosion was, in general, scarce; nevertheless, certain important details were gathered. A complete survey of tropical climates and effects was given in the report of the Army Air Forces Tropical Science Mission (40)*. In general, the tropics are characterized by high-atmospheric humidity at moderately high-atmospheric temperatures. Because of the ever present high relative humidity, condensation is prevalent during the nights. The rapid deterioration of zinc in the tropics has been traced to these conditions. Condensed moisture promotes a rapid accumulation of the zinc corrosion products. At relative humidities of 75 per cent or higher, these corrosion products are hygroscopic (26, 47) so that, even in the absence of condensed moisture, enough water apparently is absorbed to support corrosion. The failure of cadmium is probably also related to moisture condensation, but beyond this no knowledge was available.

^{*}Numbers in parentheses refer to the Bibliography in Appendix IV.

This Bibliography is the result of the literature survey and is given in its entirety.

The literature survey showed that pure metal coatings have been thoroughly exploited and indicated that there was little possibility of improvement over pure zinc or pure cadmium with the possible exception of manganese. The best chance for success appeared to be in the alloy field, with zinc or cadmium being used in binary combination with elements having better corrosion resistance.

One difficulty with many zinc and cadmium binary alloys is the small range of solid solubility. Solid solutions are, in general, more resistant to corrosion them multiphase systems.

The use of cast alloys for the survey of relative electrode potentials was visualized as being expedient. Evidence in the literature (1, 2, 6, 7, 8, 119, 120, 121, 122, 123) was not conclusive as to the magnitude of the difference, if any, of electrode potential of cast alloys from that of electrodeposited alloys of the same composition. Experiments, which are described later in this report, were performed to determine the magnitude of any difference.

Little or no effect on the corrosion resistance of zinc was observed with minor additions of various metals, (57, 62) with the exception of copper, which did make zinc more resistant (57,59). Cadmium - zinc alloys were found superior to either zinc or cadmium (65,66). Zinc - indium alloys (70), zinc - tin alloys (78, 79), zinc - nickel alloys (74), and cadmium - antimony alloys (80) were reported as being superior to zinc or cadmium in salt-spray tests. The Bureau of Mines has prepared zinc - manganese alloys, but no data were available on their corrosion characteristics.

Brown and Mears have developed the most simple and ingenious apparatus for making potential and corrosion current-density measurements (19, 20, 21).

A general discussion of alloy plating is presented in (125), and a Bibliography of alloy plating was prepared by the Fngineering Division of the Air Materiel Command of the Army Air Forces (Serial No. TSFAM - M5236).

Comparison of the Electrode Potentials of Cast and Electrodeposited Alloys, Static Electrode Potential Measurements of Electrodeposited Alloys and Pure Metals

Zinc - Copper Alloys

Static electrode potentials of cast and electrodeposited zine - copper alloys were measured in 3 per cent sodium chloride solution.

Relatively little difference (the average was approximately 30 millivolts) was observed between the potentials of the two forms. (Figure 5, Appendix II, Tables 1 and 3, Appendix III). The observed differences are not significant when it is considered that the alloy containing as much as 28 per cent copper is approximately 300 millivolts less noble than SAE X-4130 steel, which is-0.706 volt on the calomel scale.

Two pairs of zinc - copper specimens, each pair consisting of one cast and one electrodeposited alloy having the same or very nearly the same composition, were tested for corrosion current density and polarization characteristics, when coupled to specimens of SAE X-4130 steel and immersed in an electrolyte of 3 per cent sodium chloride solution at 90°F. The alloys of the same composition showed corrosion current densities and polarization characteristics very much the same regardless of whether they were electrodeposited or cast (Figure 6, Appendix III, Table 4, Appendix III).

Zinc - Tin Alloys

The static potentials of the zinc - tin alloys in 3 per cent sodium chloride solution show good agreement with those of the cast alloys (Figure 32, Table 39) up to 50 per cent tin. From this point on, the electrodeposited alloys become noble more rapidly than do the cast alloys.

Cadmium - Silver Allovs

Static electrode potentials of two alloys, containing 2.95 per cent and 5.75 per cent silver, respectively, were measured in 3 per cent sodium chloride solution (Table 39), and were in good agreement with the cast alloys being some 20 millivolts less noble than the corresponding cast specimens.

Zinc - Lead Alloys

Two alloys, containing 13.3 per cent and 17.7 per cent lead, respectively, showed potentials within a few millivolts of pure zinc when measured in 3 per cent sodium chloride solution (Table 39).

Porous Zinc Electroplate

The static potentials of porous zinc plate with and without chromate treatment were measured in 3 per cent sodium chloride solution (Table 40). Untreated porous zinc plate is but slightly less noble than cast zinc. With the chromate treatment, the potential becomes approximately 30 millivolts more noble.

Manganese

The potential of electrodeposited manganese in 3 per cent sodium chloride solution (Table 40) is approximately 200 millivolts less noble then that of zinc. The potential becomes more noble with time. (See also Table 27).

Conclusions

Following the results of comparing cast and electrodeposited high zinc - copper alloys, the decision was made to use cast alloys for the electrode potential measurements in first separation of likely from unlikely alloys. The results with the cast alloys are summarized in the immediately following major section of this report.

After that series of measurements with cast alloys, the abovementioned data were obtained for additional checks with the electrodeposited alloys of zinc - tin, cadmium - silver, and zinc - lead. Porous
zinc plate and electromanganese were included in this series of tests on
the electrodeposited alloys.

Static and Dynamic Potential and Corrosion Current Density Measurements of Fourteen Cast Binary Alloy Systems

Following the decision to use cast alloys for electrode potential measurements, specimens were prepared representing thirteen binary systems. The methods of preparation are described in Appendix I. The static potentials were measured in 3 per cent sodium chloride solution, in water saturated with carbon dioxide, and in distilled water, at 90°F. against

saturated calomel electrodes. From these measurements were drawn the conclusions as to whether an alloy could be expected to protect steel sacrificially.

The dynamic measurements were made in 3 per cent sodium chloride solution at 90°F. These measurements provided information relative to polarization and corrosion current density as influenced by alloying. In developing substitute alloys, it is desired to provide the lowest possible corrosion current-density commensurate with sacrificial protection. Such alloys should also retain an electrode potential appreciably less noble than that of steel. The larger the difference the more effective will the alloy coating be in protecting "bare" areas of steel. Alloys more noble than steel will not give the kind of protection desired in this work. In the following discussions, "less noble" is used synonymously with "anodic to steel", and "more noble" with "cathodic to steel". The 24-hour corrosion current densities are close to the equilibrium values and were used in determining the relative worth of the alloys under corroding conditions.

Appendix II contains graphs of the static and dynamic potential and corrosion current density data. The tables which contain the time. potential data and the dynamic data are found in Appendix III.

Alloys Considered Prospects for Further Study

On the basis of electrode potential data, the following systems contain alloys that are considered prospects for further study.

Zinc - Copper Alloys. In the range studied, up to 30 per cent copper, these alloys are less noble (retention of protective tendency) than steel in 3 per cent sodium chloride solution (Figure 5, Tables 1 and 2), and in water saturated with carbon dioxide (Figure 22, Table 21). In distilled water, however, the potential becomes more noble (loss of protective tendency) than that of steel at approximately 17 per cent copper (Figure 18, Table 15).

Increase in copper content lowers the corrosion current density, so that, at 28 per cent copper, the current density is approximately one-half that of pure zinc (Figure 6, Table 4) in the sodium chloride solution.

Gadmium - Zinc Alloys. This system is anodic to (less noble than) steel over the entire composition range in 3 per cent sodium chloride solution (Figure 7, Table 9), and in water saturated with carbon dioxide (Figure 24, Table 25). In distilled water, the alloys become cathodic to (more noble than) steel at approximately 65 per cent cadmium. (Figure 20, Table 19) The corrosion current density decreases uniformly with increase in cadmium content and reaches its lowest value at 90 per cent cadmium (Figure 13, Table 13) in the sodium chloride solution.

Zinc - Silver Allovs. In 3 per cent sodium chloride solution, and in water saturated with carbon dioxide, zinc - silver alloys are anodic to (less noble than) steel where the silver content does not exceed 29 per cent (Figure 7, Table 8, and Figure 24, Table 24). Alloys containing more than 28 per cent silver are cathodic. In distilled water, the

effect of silver is more marked, since a 5 per cent addition to zinc causes the alloy to be cathodic to steel (Figure 20, Table 18), the transition from the anodic side taking place at about 4 per cent silver. Silver causes a pronounced effect on the corrosion current density in 3 per cent sodium chloride solution where a 25 per cent silver alloy has a current density less than one-half that of pure zinc (Figure 11, Table 12).

Cadmium - Silver Alloys. Cadmium - silver alloys are anodice to steel in 3 per cent sodium chloride solution if they contain less than 18 per cent silver. At 18 per cent silver, they reverse and become cathodic to steel (Figure 7, Table 8). In carbon dioxide saturated water, the transition from anodic to cathodic relationship occurs at about 16 per cent silver (Figure 24, Table 24). In distilled water, the entire cadmium - silver system is cathodic to steel (Figure 20, Table 18). The dynamic measurements in 3 per cent sodium chloride solution show a slight decrease in corrosion current density (Figure 11, Table 12) and also show that protection is not given to the steel if the silver exceeds 8 per cent.

Zinc - Tin Alloys. Zinc - tin alloys, containing up to 95 per cent tin, are anodic to steel in 3 per cent sodium chloride solution (Figure 9, Tables 5, 11) and in water saturated with carbon dioxide (Figure 23, Table 22). It is also observed in Figure 9 that the as-cast specimens have potential values almost identical with those of the machined specimens. At approximately 35 per cent tin, zinc - tin alloys become more noble than steel in distilled water (Figure 19, Table 16). The 24-hour corrosion current-density curve (Figure 17, Tables 7, 13) shows

the large drop in current density in 3 per cent sodium chloride solution, due to increase in tin content. The current density for the 90 per cent tin alloy is approximately one-fourth that of pure zinc.

Zinc - Nickel Alloys. Zinc - nickel alloys, through 12 per cent nickel, are less noble than steel in 3 per cent sodium chloride solution, $^{\rm CO}_{2^-}$ saturated water, and distilled water (Figure 26, Table 33). At some point between 12 per cent nickel and 47 per cent nickel, the alloys become cathodic to steel. This point was not determined because the alloys having compositions between these points were very brittle and specimens could not be prepared by melting and casting techniques. A gradual decrease in current density is observed with increase in nickel (Figure 33, Table 41), so that, at 12 per cent nickel, the current density is half that for pure zinc in the sodium chloride solution.

Zinc - Chromium Allovs. Zinc - chromium alloys, through 5.36 per cent chromium, are anodic to steel in 3 per cent sodium chloride solution, CO₂—saturated water, and distilled water (Figure 30, Table 37). Slight changes are observed in the potential with small additions (0.5 per cent to 2 per cent) of chromium. An appreciable lowering of the current density in 3 per cent sodium chloride solution is observed (Figure 38, Table 41) with increase in chromium.

In the present work, this system was limited to the composition range given because of difficulties attendant upon the melting technique. This system has no known method for alloy electrodeposition, but, in case of outstanding prospects, a deposition study can be justified.

Zinc - Manganese Allovs. Through 9.6 per cent manganese, these alloys are anodic to steel in 3 per cent sodium chloride solution, CO₂-saturated water, and distilled water (Figure 31, Table 38). The current density gradually decreases with increase in manganese up to about 5 per cent (Figure 40, Table 42). From 5 per cent to 9.6 per cent, there is a slight rise in current density. This system was also limited in the present work, because of melting difficulties.

Alloys Showing Little or No Prospects or Incompletely Studied

Electrods potential data show that the following alloys are unlikely to be improvements over pure zinc or pure cadmium, or the systems have not been completely investigated to date.

Zinc - Lead Alloys. Because of the very limited miscibility of zinc and lead, alloys of these two elements could not be prepared by casting beyond one per cent at either end of the constitution diagram. Alloy preparation by electrodeposition methods appears more promising. One per cent lead in zinc does not appreciably affect the potential in 3 per cent sodium chloride solution, CO₂— saturated water, and distilled water (Figure 28, Table 35), the alloys being less noble than steel in all three media.

At 99 per cent lead, the potentials in CO₂-saturated water and distilled water are more noble than that for steel, while, in 3 per cent sodium chloride solution, the potential is less noble than that of steel. This latter result is due to a slow attainment of equilibrium of the high-lead alloy. The 24-hour corrosion current-density curve (Figure 36,

Table 42) shows a slight decrease in current density as the lead increases up to one per cent.

Cadmium - Lead Alloys. Lead in amounts up to 13 per cent does not influence the potential of cadmium - lead alloys in 3 per cent sodium chloride solution and CO₂-saturated water. In distilled water, a change of approximately 200 millivolts in the more noble direction takes place with the addition of 2 per cent lead to the cadmium (Figure 29, Table 36), with further additions causing only a slight change to less noble values. No change in corrosion current density in 3 per cent sodium chloride solution is observed with addition of lead (Figure 36, Table 42) to cadmium.

Cadmium - Tin Alloys. The cadmium - tin alloys are less noble than steel in 3 per cent sodium chloride solution if the tin content does not exceed 80 per cent (Figure 9, Table 6). In water saturated with carbon dioxide, tin does not cause the alloys to become more noble than steel until its content reaches 95 per cent (Figure 23, Table 23).

In distilled water, the entire cadmium - tin series is more noble than steel (Figure 19, Table 17). Tin up to 80 per cent appears to have little effect on the corrosion current density in 3 per cent sodium chloride solution (Figure 17, Table 7).

<u>Cadmium - Nickel Allovs</u>. Thus far, these alloys have been investigated over a very narrow composition range, because of the difficulty of preparing them thermally. Through 2.75 per cent nickel, the alloys are anodic to steel in 3 per cent sodium chloride solution and .

CO₂-saturated water, but, in distilled water, they are cathodic to steel

(Figure 27, Table 34). No significant change in current density, in sodium chloride solution, was observed due to the addition of nickel (Figure 34, Table 41).

Zinc - Indium Allovs. Additions of indium to zinc in amounts up to 40 per cent have essentially no effect on the static potentials in 3 per cent sodium/solution (Figure 8, Table 10) or in water saturated with carbon dioxide (Figure 25, Table 26). In distilled water, indium causes the potential to become 200 millivolts less noble with a 3.0 per cent addition (Figure 21, Table 20), but further additions have little effect. The twenty-four-hour curve (Figure 15, Table 14) shows that, up to 40 per cent indium, the corrosion current density is the same as that for zinc.

Cadmium - Indium Alloys. The cadmium - indium alloys, containing

3 per cent or more indium, have potentials which are a few millivolts less
noble than steel in 3 per cent sodium chloride solution (Figure 8, Table

10). In water saturated with carbon dioxide, the addition of one per cent
indium to cadmium causes the potential to become more noble than that of
steel (Figure 25, Table 26). The cadmium - indium alloys are rore noble
than steel when immersed in distilled water (Figure 21, Table 20). Indium
in amounts greater than 10 per cent causes a slight drop in corrosion
current density (Figure 15, Table 14) in 3 per cent sodium chloride solution,
but none of the alloys tested gave complete protection to the steel. Small
amounts of iron rust were observed in each case.

Pure Metals

The static potentials of the cast pure metals are found in Tables 27 and 28.

Tests in "Wet-Dry Program" Cabinet

The "wet-dry program" cabinet was designed to provide a period of condensation followed by a period of dryness, simulating the tropical conditions.

The cadmium - tin and cadmium - zinc cast alloys were tested first. The initial cycling was arbitrary and consisted of a condensation period of 25 minutes and a dry period of 11 minutes. During the condensation period, the air temperature was in the range 115° - 120°F., while, for the dry period, it was between 65°F. and 75°F. This is recognized as not exactly duplicating tropical conditions, but is believed to be sufficiently comparable for this initial work. After 162 hours and 275 cycles, the specimens were removed and examined. The corrosion resistance of the cadmium - tin alloys appeared to be equal to that of pure cadmium. With the cadmium - zinc series, there was a definite correlation between composition and corrosion resistance, the attack being least on the high-cadmium alloys and heaviest on the high-zinc alloys.

Cast zinc - nickel and cadmium - nickel specimens were exposed for 383 hours and 582 cycles (the dry period had been increased to 14-1/2 minutes). The zinc - nickel alloys with 12 per cent nickel showed less corrosion than those with lower nickel contents, one of which contained only 0.03 per cent nickel and probably can be considered equal to pure zinc in corrosion properties. In the case of the cadmium - nickel alloys, no improvement over pure cadmium was observed for alloys containing up to 3 per cent nickel.

Also exposed were specimens plated with porous zinc that had received a chromate passivating treatment and specimens coated with regular zinc plate that had also received a chromate treatment. Before being placed in the cabinet, each of the specimens was scratched with a file to expose some of the metal coating beneath the passivated surface. After 499 hours and 758 cycles, the regular zinc plate with chromate passivated surface showed no corrosion whatsoever, either in the scratches or elsewhere. The porous zinc plate, which had also received the passivation treatment, had "moderate to heavy" corrosion in the scratches and "slight to moderate" corrosion in general.

Corrosion Test Check of Static Electrode Potential Values for Distilled Water

To test the relative value of static potential measurements made in distilled water, two cast alloy systems, the zinc - tin and the cadmium - zinc (Figures 19 and 20), were chosen for further experiments. A series of galvanic cells was set up, using X-4130 steel and specimens of the two above-mentioned allow systems. These couples were immersed in distilled water and held at 90°F, for 24 hours. Examination at the end of this period showed that, in every case where an alloy did not protect the steel, the static electrode potential measurements (again see Figures 19 and 20) showed values more noble than those for the steel.

EXPERIMENTAL*

The apparatus and methods used for this project are described in detail in Appendix \mathbf{I}_{\bullet}

^{*}Laboratory Record Book No. 2875, pp. 1-100. Laboratory Record Book No. 31°0, pp. 1-100. Laboratory Record Book No. 3363, pp. 1-30. Laboratory Record Book No. 3393, pp. 1-14. Laboratory Record Book No. 3942, pp. 1-23.

APPENDIX I

This Appendix contains descriptions of all apparatus and all methods used for this project.

Prenaration of the Media in Which Electrode Potentials Were Measured

Three Per Cent Sodium Chloride Solution

The water used for the sodium chloride solution was the regular laboratory distilled water having a pH of 6,3 The salt used was "Baker's Analyzed", chemically pure sodium chloride. The solution was filtered and the concentration checked by accurate specific gravity measurement.

Distilled Water

The distilled water, which was used alone for potential measurements, was a specially purchased product having a specific conductivity of 5×10^{-6} reciprocal ohms and a pH of 6.9 - 7.0. It was protected by a tube containing "ascarite", a carbon dioxide absorbing substance.

Distilled Water Saturated with Carbon Dioxide

Bottled carbon dioxide was bubbled through the special distilled water. At the end of one hour, the pH was 4.1, and further treatment with carbon dioxide did not change the pH. Lundell and Hoffman* give 3.7 as the pH of water saturated with carbon dioxide. The 4.1 value *"Outlines of Methods of Chemical Analysis", John Wiley and Sons, 1938, p. 133.

was reproducible in the present work, however, and numerous checks showed no deviation from this value.

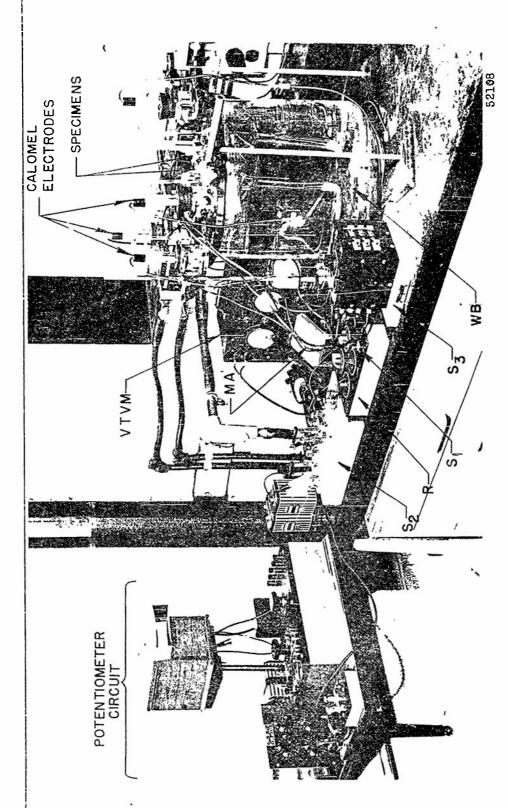
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Static Electrode Potential Measurements

Apparatus

Figure 1 is a picture of the apparatus as set up for measuring static electrode potentials of four specimens concurrently. Also pictured in this figure are the additional pieces of equipment used in the dynamic measurements which are described later.

Northrup student-type potentiometric circuit. No. 4970 saturated calomel cells, designed for use with the Beckman pH meter*, were used as reference electrodes. When measurements were made in distilled water or distilled water saturated with carbon dioxide, the calomel electrodes dipped directly into these media. For the measurements in 3 per cent sodium chloride solution, the calomel electrode dipped into a small cup containing a saturated solution of potassium chloride. A bent, 7-mm. - diameter glass tube, containing a 3 per cent sodium chloride solution, connected this cup to the beaker filled with a 3 per cent solution of sodium chloride, into which dipped the specimen. The end of the glass tube, which dipped into the 3 per cent sodium chloride solution, was drawn down to a small bore and a 5-mm. length of fibrous asbestos was sealed in. The asbestos tip reduced diffusion and, by having the calomel *Manufactured by the National Technical Labs., Fasadena, California.



Apparatus for the measurement of static and dynamic electrode potentials and corrosion currents. As pictured, the apparatus is connected to measure static electrode potentials. Figure 1.

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electrode dip into the saturated potassium chloride solution, contamination of the calomel electrode by sodium ions is minimized.

The corrosive media were contained in 250-ml. beakers. The beakers were immersed in a thermostatically controlled water bath

(WB in Figure 1) which operated within ± 1°F. of the desired temperature.

The specimens were supported in bakelite clamps which rested on the edges of the beakers. A four-way rotating double-pole switch (S₃ in Figure 1) was used so as to make possible the concurrent measurement of four specimens.

The potentiometric circuit was calibrated twice by the Battelle instrument laboratory and was found to be correct.

Method

The calomel electrodes were placed so that the dips dipped into the corrosive medium to a depth of 3/4 inch. The clamped specimens were then immersed vertically to a depth of 1-1/2 inches and placed so as to be 1/4 inch from the calomel electrode tips. After one minute, the initial potential measurement was made (except for measurements in distilled water. See below. Subsequent measurements were then made at five-or ten-minute intervals following the instant of immersion. The total elapsed time, in most cases, did not exceed 60 minutes. In the cases of several pure metals, the elapsed time ran as high as 160 minutes, since the rate of change of potential with time was still rapid at 60 minutes.

When the specimens were being tested in distilled water, the initial measurements were made after 60 minutes had elapsed and subsequent measurements were made at 75 minutes and 90 minutes. The reason for waiting 60 minutes before making the initial measurement was to allow a small amount of metallic material to dissolve, thus increasing the conductivity. The calomel electrodes were removed from the water when measurements were not being made, so that no contamination would result from potassium chloride.

In making the measurements, care was taken to tap the circuitclosing key, but momentarily, in order to minimize polarization.

Dynamic Potential and Corrosion Cell Current Density Measurements

Apparatus

The circuit developed by Brown and Mears*, for measuring potentials and currents in coupled cells, was used in this work. A schematic diagram of this so-called "zero resistance" circuit is given in Figure 2. As shown in Figure 1, the apparatus was connected for measurement of static electrode potentials. By disconnecting the potentiometer leads from the four-way switching box and reconnecting them to terminals 2 and 5 of S₂ (Figure 2), and connecting two calomel electrodes as shown in Figure 2, the apparatus was ready for dynamic measurements. MA (the code letters refer to Figures 1 and 2) is a 0-10 milliammeter. The battery between resistance R and S₁ in Figure 2, was a 1-1/2-volt dry cell.
*Trans. Flectrochem. Soc., 74, 495 (1938)

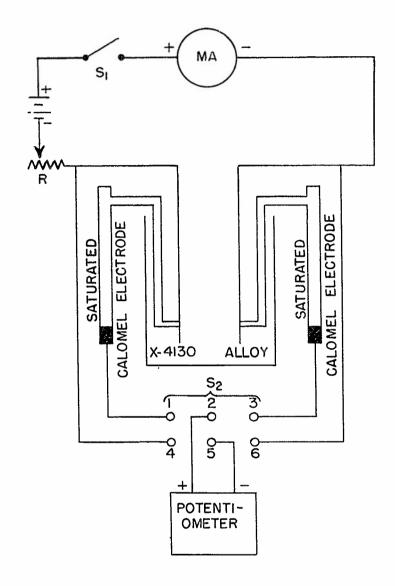


FIGURE 2 - SCHEMATIC REPRESENTATION OF THE "ZERO RESISTANCE" CIRCUIT FOR MEASUREMENT OF CORROSION CURRENTS AND ELECTRODE POLARIZATION

Resistance R comprised a 5000-ohm, a 3000-ohm, and two 1000-ohm variable radio potentiometers connected in series. Switch S₂ was constructed from two knife switches, one a double-pole double-throw type, and the other a double-pole single-throw type. In addition to the Leeds and Northrup potentiometer circuit, a simple slide back, vacuum tube voltmeter was used for rough measurements, and preliminary adjustments (WTVM in Figure 1).

The specimens were supported by bakelite clamps, which held the steel and alloy one inch apart. The alloy specimens measured 1 inch x 3 inches, while the steel specimens measured 1 inch x 4 inches. The specimens dipped into the solution 1-1/2 inches.

Method

The clamped specimens were immersed in the sodium chloride and were then connected in the circuit. Two calomel electrodes were placed so that the tips pressed against the surfaces of the steel and alloy, respectively. A period of twenty minutes elapsed, following the instant of immersion, and the measurements were made according to the following procedure:

- 1. With Switch S_1 open, and Switch S_2 thrown so that contacts 1 and 4 were connected to 2 and 5, respectively, the potential of the X-4130 steel was measured.
- 2. With Switch S₁ open, and S₂ thrown, so that contacts 3 and 6 were connected to 2 and 5, respectively, the potential of the alloy was measured.

- 3. With S₁ open, and S₂ thrown, so that Contacts 4 and 6 were connected to 2 and 5, respectively, the difference in potential between the steel and alloy was measured. This value should be very close to the calculated difference obtained from Steps 1 and 2.
- 4. With S₂ thrown as in Step 3, S₁ was closed and Resistance R was adjusted, so that the potential difference between the steel and alloy was zero. The corrosion current for the cell was then read on the milliammeter.
- 5. With S_1 closed, the separate potentials of the steel and alloy were measured as in Steps 1 and 2.

Preparation of Cast Allovs

Low-Melting Alloys

The low-melting alloys were prepared directly in a gas-fired crucible furnace. This furnace was composed of a fire clay crucible which fitted in a larger graphite crucible. The latter had a one-inch hole drilled in the side wall near the bottom, through which passed the nozzle of a blast burner. The flame swirled around the inner crucible, thus distributing the heat.

Measured amounts of two chemically pure metals were placed in the inner crucible and were covered with charcoal. During melting, the inner crucible was covered and the outer crucible partly covered. After melting was complete, the temperature was maintained for 10 - 15 minutes

(in the case of the zinc - copper alloys, the temperature was maintained for approximately one hour). The melt was then stirred thoroughly with a carbon rod and poured into a carbon mold. The ingots measured 1 inch \times 3 inches \times 1/8 inch.

High-Melting Alloys

The technique described in the previous section was inadequate in the case of zinc - chromium and zinc - manganese. These alloys were prepared as follows: For the zinc - chromium system, "master" alloys were first prepared by placing zinc in an alundum thimble crucible and melting it in an induction furnace. The melt was covered with a zinc chloride flux and heated to 1520°F. One-hundred-mesh chromium powder was then stirred into the flux and finally into the melt. The resulting alloys were poured at 1510°F. Two "master" alloys, containing 12.4 per cent and 15.2 per cent chromium, respectively, were prepared in this way.

Essentially the same procedure was used in the preparation of the zinc—manganese "master" alloys. Small chips of electrolytic manganese were added to the molten zinc at 1480°F. The temperature was then raised and the pouring was done at 1620°F. The two "master" alloys contained 17.6 per cent and 19.2 per cent manganese.

In each case, the alloys which were used for measuring potentials were prepared by use of the "master" alloys in the gas-fired crucible furnace.

Preparation of Specimens for Potential Measurements

The ingots were machined on a shaper so as to produce a smooth surface. The same specimens were used for measurements in several media. Between measurements, the corrosion products were removed by light rubbing with fine steel wool. The machined surfaces of the specimens facilitated this and no significant change resulted from such light reworking of the original surface. The specimens were then cleaned by rubbing with a clean cloth saturated with carbon tetrachloride. This was followed by vapor degreasing in trichlorethylene. The steel specimens received the same treatment, but, in addition, were pickled for 20 seconds in 1-1 hydrochloric acid solution just prior to using.

Corrosion Test Check of Static Electrode Potential Values for Distilled Water

The cells contained an X-4130 cathode 1/16-inch thick and 1/4-inch wide. Facing this cathode on each of two sides and spaced 1/16-inch from it was a cast alloy anode one inch wide and 1/8-inch thick.

An anode to cathode area ratio of 8 to 1 and the 1/16-inch spacing, were experimentally determined as being necessary if rusting of the cathode, when coupled to a less noble metal or alloy, was not to occur. With too small an area ratio and too great a spacing, even pure zinc did not protect steel in distilled water, since the minimum current density required for protection was not reached. The anodes and cathodes were immersed in distilled water to depths of 1-1/2 inches and 1-3/8 inches, respectively, and were coupled with short external "jumpers". The

distilled water was contained in 250-ml. beakers, and the electrodes were held in place by bakelite clamps, which rested on the edges of the beakers.

Preparation of Electrodeposited Alloys

Zinc - Copper Electrodeposits

Steel specimens were degreased in trichlorethylene vapor, followed by an anodic treatment for one minute in Anodex* at 5 volts and 190°F. A 30-second dip in 1-1 hydrochloric acid solution at room temperature, a thorough washing, and a quick dip in dilute KCN solution completed the pretreatment.

In the early experiments, a bath described by Oplinger** was used. This bath was developed to plate an alloy containing 26 per cent to 29 per cent copper and has the following composition:

NeCN 90 g./1.
CuCN 18 g./1.
Zn(CN)₂ 70 g./1.
NaOH 70 g./1.

Temperature - 105°F.

Current Density - 20 amp./sq. ft.

By using pure zinc anodes and "dummying" the bath for various periods of time, the solution was depleted in copper, and specimens within the desired composition range were produced.

*MacDermid, Inc., St. Louis, Missouri.

**Met. Ind. (N. Y.) 36, 513, 1938.

This method was soon found to be too slow, so a stock zinc plating solution was prepared. By adding copper cyanide in various quantities to the stock solution, alloys of different compositions were deposited. The stock solution was as follows:

NaCN

90 g./1.

Zn(CN)2

70 g./1.

NaOH

70 g./1.

The plating conditions were the same as for the Oplinger bath.

Zinc - Tin Electrodeposits

These were plated from an alkaline stannate - zinc cyanide bath, as described by R. M. Angles (J. Electrodepositors' Tech. Soc., 21, 45, 1946). SAE X-4130 steel specimens, measuring 1 inch x 4 inches, which had been polished on a 240-emery belt, were cleaned for one minute cathodically and one minute anodically in Anodex at 190°F. and 100 amp. sq. ft. This cleaning was followed by a three-minute dip in 6-N. hydrochloric acid at room temperature. The specimens were then electroplated according to the conditions given in Table 31, Appendix III. Alloy anodes of composition 20 per cent zinc - 80 per cent tin were used in all cases. No agitation was used.

Cadmium - Silver Electrodeposits

The bath developed by C. L. Faust, D. J. Henry, and W. G. France (Trans. Electrochem. Soc., 72, 479, 1937) was used for the two cadmium - silver alloys.

Specimens of SAE X-4130 steel were prepared in the same way as described for the zinc - tin alloys. The specimens were then plated as shown in Table 32, Appendix III, using steel anodes. No agitation was used.

Zinc - Lead Electrodeposits

Very little information on the electrodeposition of zinc - lead was available. Mason (U. S. Patent 2,136,629) described a method of codepositing small amounts of lead with zinc, in order to increase the stain resistance of zinc. He used an alkaline bath with gum Arabic and sodium fluoride as addition agents. In the present work, alloy deposits, containing from 5 per cent to 86 per cent lead, were produced from an alkaline tartrate bath. The compositions of the deposits varied widely even when plating conditions were apparently identical.

Pretreatment for the SAE X-4130 steel panels consisted of an anodic treatment in Anodex* at 190°F, and 25 amp./sq. ft. for one minute, followed by a 15-second dip in 3-N hydrochloric acid at room temperature.

The bath composition and the conditions for plating were as follows:

Zn(CN) ₂	90 g./1.
Na OH	96 g./1.
NaCN	37.5 g./1.
KNaC4H4O6°4H2D	1.2 g./1.
Pb(C_H_O) OH	2.5 g./l.

*Mac Dermid, Inc., St. Louis, Missouri.

Gum Arabic

0.75 g_e/1.

NaF

4 g./l.

RH 774*

1.8 to 6.8 g./1.

Temperature

75 - 85°F.

Current Density

3.5 amp./sq. ft.

No agitation

Steel anodes

The 13 per cent lead alloy and the 18 per cent lead alloy were plated from the same bath, the only difference being that, for the former, the bath contained 6.8 g./l. RH-774*, while, for the latter, the RH-774 content was 1.8 g./l.

Procedure for Depositing Porous Zinc Plate

Electroplating Bath

ZnS04*7H_0

360 g./1.

NaC2H3O2*2H2O

15 g./l.

NH₄Cl

30 g./1.

Aquadag** (20 per cent solids)

- --

50 g./1.

Operating Conditions

Current density

100 amp./sq. ft.

Temperature

90°F. + 2°F.

ъH

2.0 to 4.3

*Du Pont antipit agent.

**Manufactured by the Acheson Colloids Corp., Fort Huron, Michigan.

Anodes

Cast zinc

Work-bar reciprocated 66 cycles/minute

1-1/4-inch stroke

Plating time - 6 minutes

Operating Details

Duplicate SAE X-4130 steel specimens, 0.042 inch x 1 inch x 4 inches, cleaned anodically in Anodex* (75 g./1., 180°F., 100 amp./sq. ft. 2 minutes) and dipped in 10 per cent hydrochloric acid, were immersed to a depth of 3-1/2 inches in 800-ml. electroplating baths. Current was applied after immersion and was adjusted to 100 amp./sq. ft. After plating for 6 minutes, the strips were removed and the edges were brushed with a soft bristle brush to remove trees. One of each pair was tested for porosity, as described in the following section.

Method for Determining Porosity

After plating, the specimens were rinsed in boiling water, dried in an oven at 120°F., and reweighed to obtain the weight of zinc deposited. Then they were placed in an oil bath containing uninhibited oil (SAE 10) at 240°F. and evacuated to a pressure of less than 1 mm. mercury. The specimens were removed after 30 minutes, cooled in air, and, after draining on edge for 30 minutes, were weighed once more. A blank, (0.015 gram) corresponding to the weight of oil that remained on the surface of nonporous steel strips (an average of three determinations), was subtracted from the increase in weight due to oil. Porosity was then *Mac Dermid, Inc., St. Louis, Missouri.

calculated as follows:

Porosity (per cent) =
$$\frac{\text{wD}}{\text{wD} + \text{Wd}}$$

- where w was the weight of the oil in the pores
 - W was the weight of electrodeposited zinc
 - d was the density of the oil (0.890)
 - D was the density of the zinc plate (7.14)

Effect of Variation of pH on Porosity

The effect of variations in bath pH on porosity was found to be considerable and is shown in Figure 41, Appendix II. The effects of varying temperature, current density, etc., were not investigated.

Chemical Analysis

The chemical analysis of the cast alloys was accomplished using methods described in the standard texts such as:

"Applied Inorganic Analysis"

W. F. Hillebrand and G. E. F. Lundell John Wiley and Sons

"Scotts Standard Methods of Analysis"

D. Van Nostrand Company

The compositions of the electrodeposits were determined by plating duplicate cathodes of platinum or stainless steel and stripping with nitric acid. The analyses were then performed as for the cast alloys.

Electroplating solution analyses followed the methods given in "Modern Electroplating", published by The Electrochemical Society, Inc., in 1942.

The Wet-Dry Program Cabinet

A lead-lined, cork-insulated plywood box, measuring 34 inches x 25 inches x 25 inches, is the basis for the wet-dry program cabinet pictured in Figure 3. This box is equipped with a 1/2-inch-thick Lucite door (a) (letters in parentheses refer to Figure 3), on which the specimens are supported by being clamped between Lucite washers in such a way that the test pieces do not make contact with the 18-8 stainless steel machine screws passing through the washers. Twenty-four specimens can be exposed simultaneously. It was necessary to bind the edges of the Lucite door with angle iron to prevent warping.

The Lucite door is opened and closed in a predetermined cycle by a small motor (B), which, in turn, is actuated by a timing device (C) operating through relay (B). The motor (B) is a special type having two field coils, one of which "shades" the other causing reversal.

To provide high humidity when the door is closed, water in a copper pan, measuring 16 inches x 16 inches x 5 inches, is warmed by an immersion heater. The heater (electrical leads at F) is controlled by a thermostat (hidden by plate G) and operates only when the door is closed. A constant-level device (E) is connected to the copper pan. The electric fan operates when the door is opened, cooling and drying the specimens. When the door is closed again and the humid atmosphere prevails, moisture

easily condenses on the chilled specimens. A schematic drawing of the electrical circuit is given in Figure 4.

Details of Electrical Circuit for Wet-Dry Program Cabinet

The following is a list of the parts with sources:

Mator - 110-volt A.C. Crise Electric Mfg. Co., Columbus, Ohio.

<u>Time Control</u> - Iron Fireman controller, Model C200-160, Iron Fireman Mfg. Co., Portland, Oregon.

Heater - Lo Lag, 2000-watt, 230-volt copper-clad immersion heater. American Instrument Company, Silver Spring, Maryland.

Relay - Double-pole, double-throw relay. Struthers-Dunn, Inc., Philadelphia, Pa. (Note: In Figure 4, the relay was not represented as being of the DPDT type for reasons of simplicity).

Thermoregulator - 230 volts, 12 wett, using 0.1 mfd. condenser in parallel. Fenwall, Inc., Ashland, Mass.

When the relay is in position A, the door of the cabinet opens and the fan operates. When the relay is in position B, the door closes, the fan stops, and the heater operates.

CAS: A.B.T. CLF:LBF 12-12-47

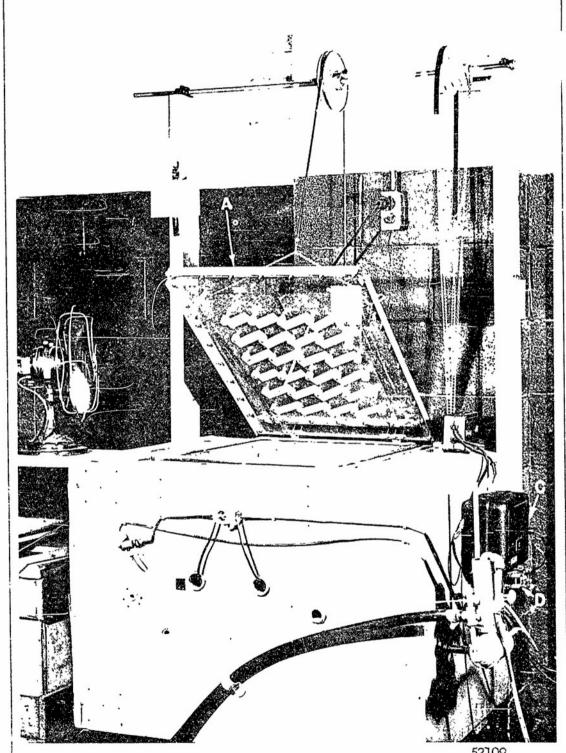
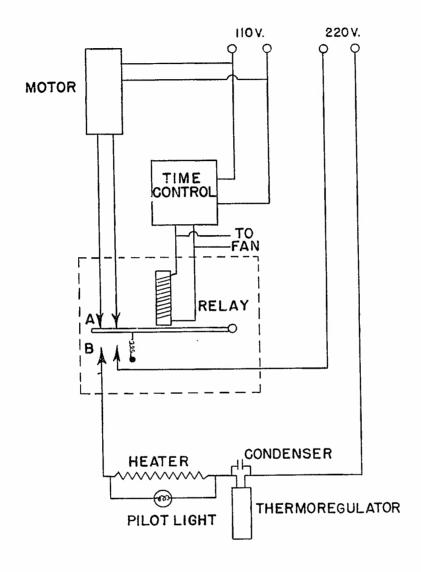


Figure 3. "Wet-Dry Program" cabinet, showing door open and corroding specimens in place



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FIGURE 4. SCHEMATIC DIAGRAM OF ELECTRICAL CIRCUIT FOR "WET-DRY PROGRAM" CABINET.

APPENDIX II

This Appendix contains the graphs of the static and dynamic potential data and the corrosion current density data.

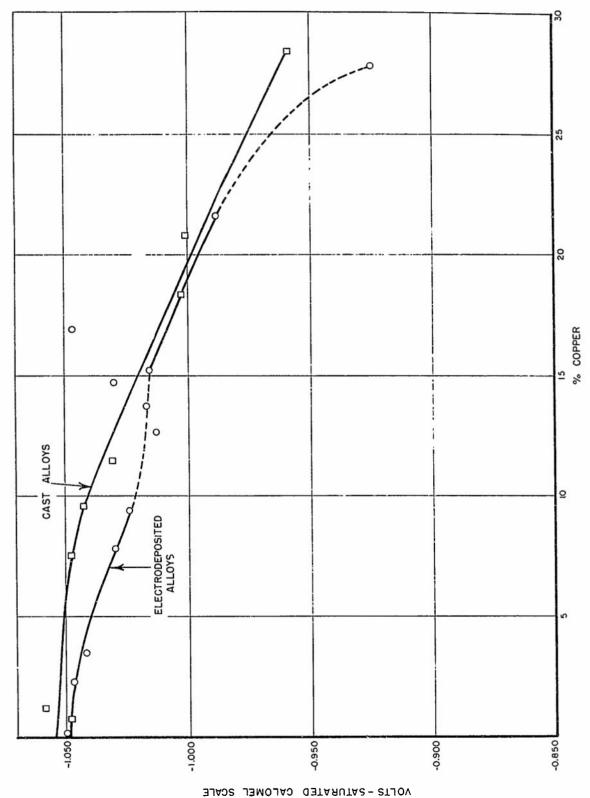


FIGURE 5 - GRAPH SHOWING POTENTIALS OF CAST AND ELECTRODEPOSITED ALLOYS IN 3% NGCI SOLUTION MEASURED AGAINST SATISATED CALOMEL CELL. ZING-COPPER ALLOYS

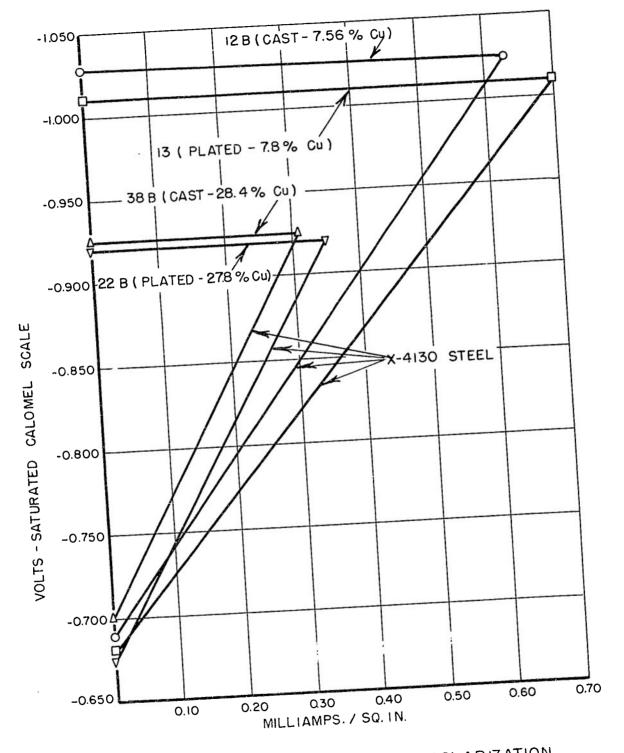
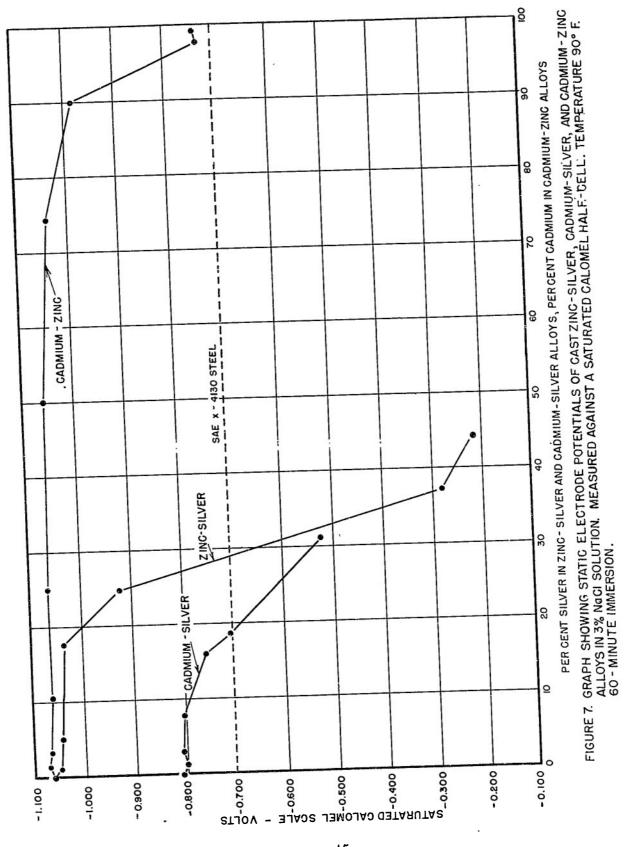
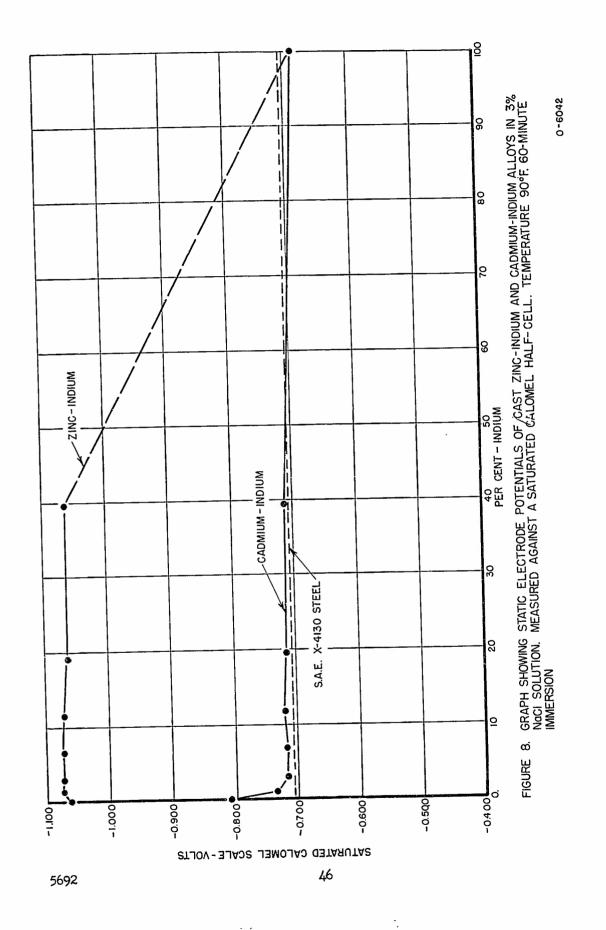


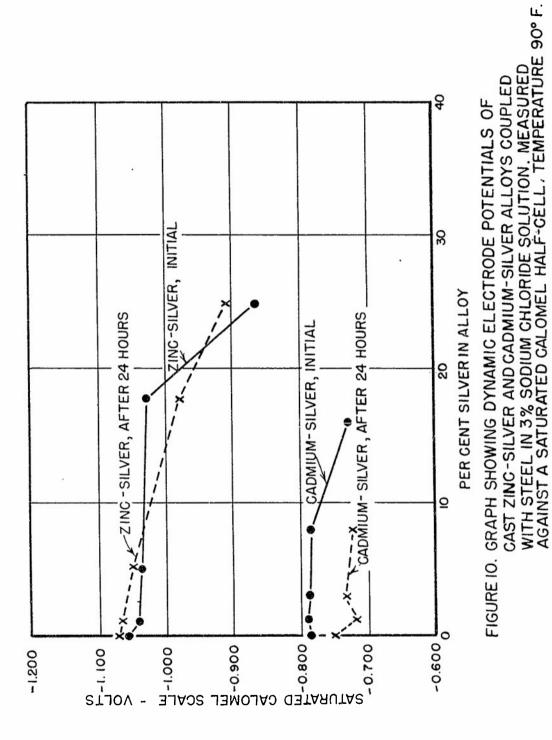
FIGURE 6 - GRAPH SHOWING SIMILAR POLARIZATION
CHARACTERISTICS AND CURRENT DENSITIES
FOR PLATED AND CAST WHITE BRASS
ALLOYS



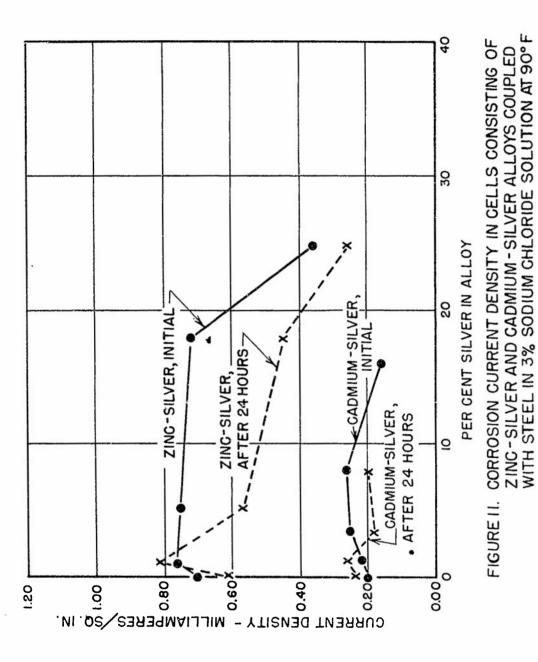


GRAPH SHOWING STATIC ELECTRODE POTENTIALS OF CAST ZING-TIN AND CADMIUM-TIN ALLOYS IN 3% NGCI SOLUTION. THIS IS FIGURE 4 OF PROGRESS REPORT NO.3 WITH THE HIGH-TIN END OF THE ZING-TIN CURVE ADDED 001 ZINC-TIN SA.E. X-4130 STEEL CADMIUM-TIN X — AS—CAST SURFACE O— MACHINED SURFACE × 30 LEGEND: -1.100 -1.000 -0.900 -0.800 C -0.700 STURATED CALOMEL SCALE-VOLTS -0.500 -0.400 FIGURE 9. 47

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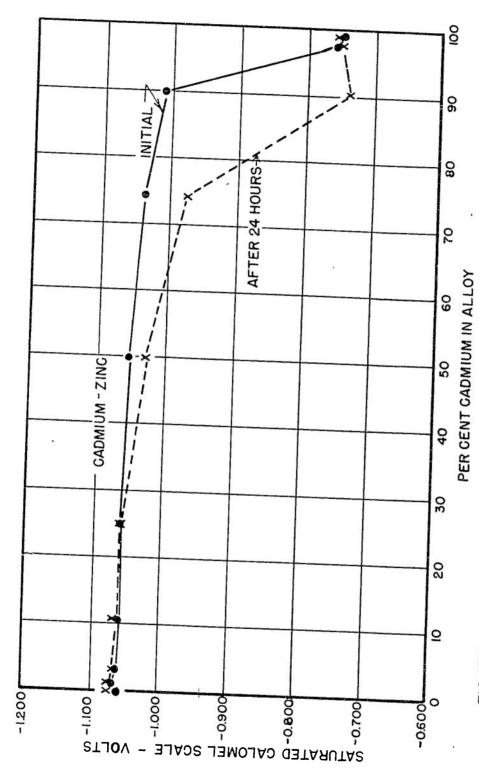
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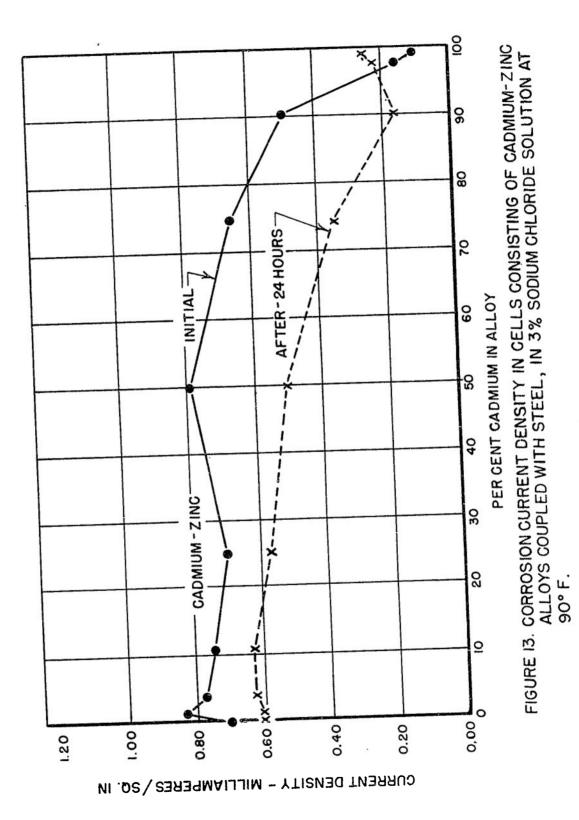
11.7



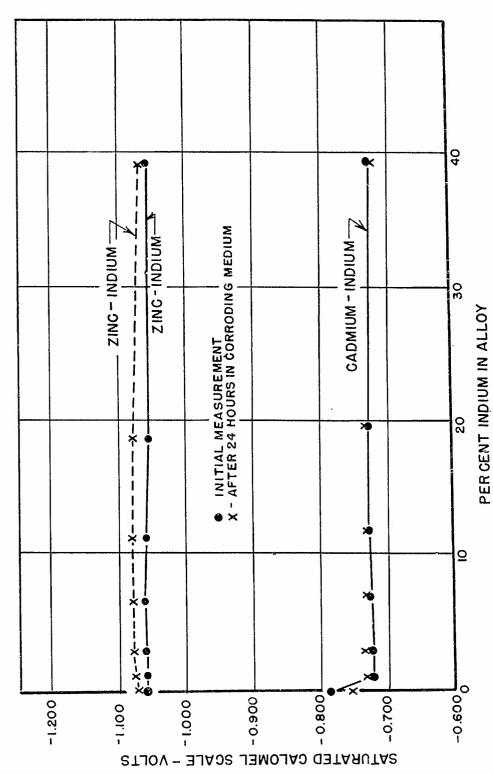
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GRAPH SHOWING DYNAMIC ELECTRODE POTENTIALS OF CAST CADMIUM -ZINC ALLOYS COUPLED WITH STEEL IN 3% SODIUM CHLORIDE SOLUTION. MEASURED AGAINST A SATURATED CALOMEL HALF-CELL, TEMPERATURE 90° F. FIGURE 12.



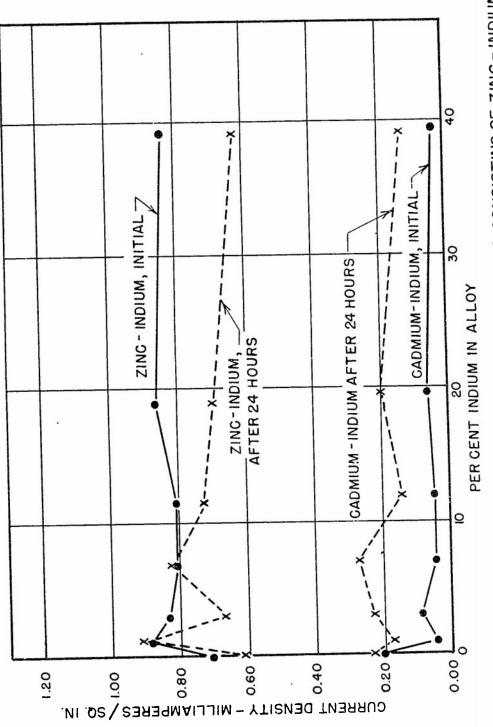
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SODIUM CHLORIDE SOLUTION. MEASURED AGAINST A SATURATED CÁLO-MEL HALF-CELL. TEMPERATURE 90° F. GRAPH SHOWING DYNAMIC ELECTRODE POTENTIALS OF CAST ZINC-INDIUM AND CADMIUM - INDIUM ALLOYS COUPLED WITH STEEL IN 3% FIGURE 14.

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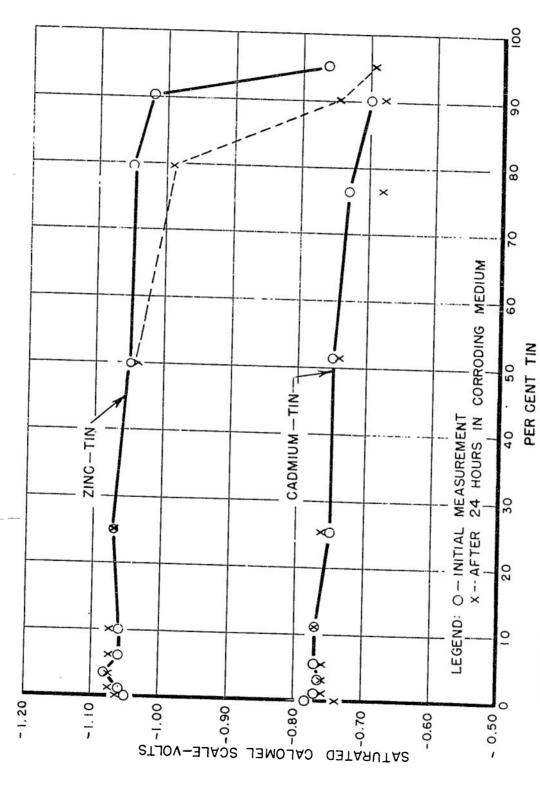


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CORROSION CURRENT DENSITY IN CELLS GONSISTING OF ZINC - INDIUM AND CADMIUM - INDIUM ALLOYS COUPLED WITH STEEL, IN 3% SODIUM CHLORIDE SOLUTION AT 90° F. FIGURE 15.

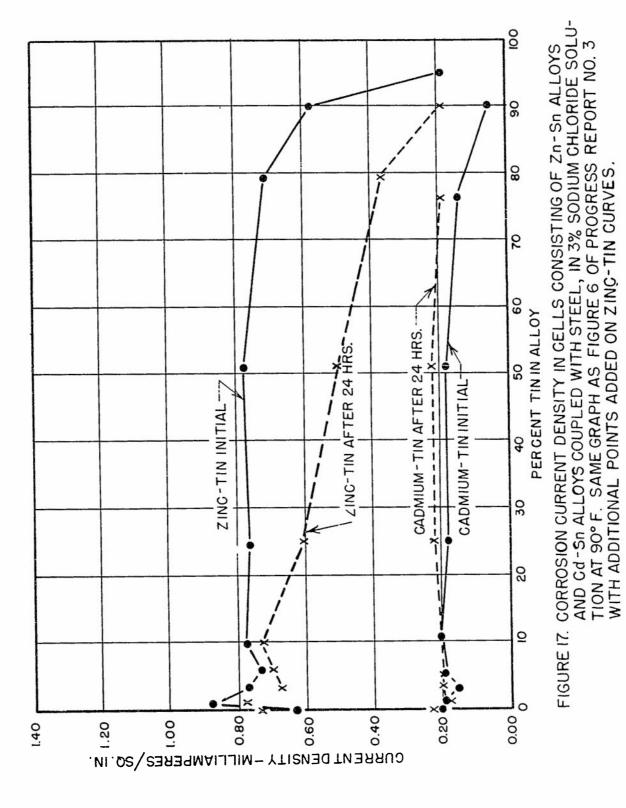
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TIN ALLOYS COUPLED WITH STEEL IN 3% NGCI SOLUTION. MEASURED AGAINST A SATURATED CALOMEL HALF-CELL. TEMPERATURE 90°F. SAME GRAPH AS FIG. 5 OF PROGRESS REPORT NO.3 WITH ADDITIONAL POINTS ADDEDON ZING-TIN CURVES. FIGURE IG. GRAPH SHOWING ELECTRODE POTENTIALS OF CAST ZINC-TIN AND CADMIUM-



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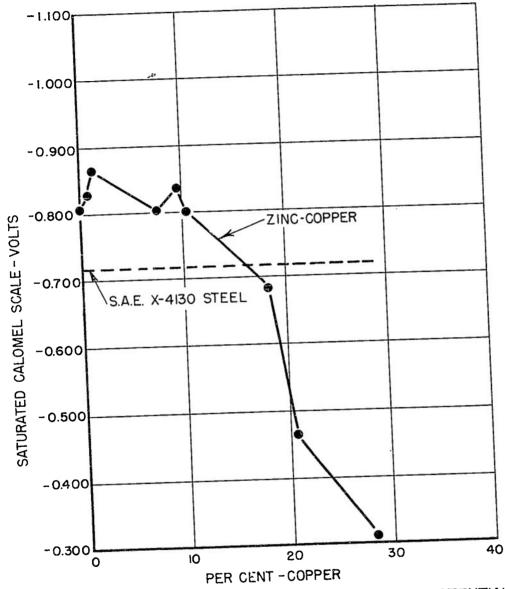
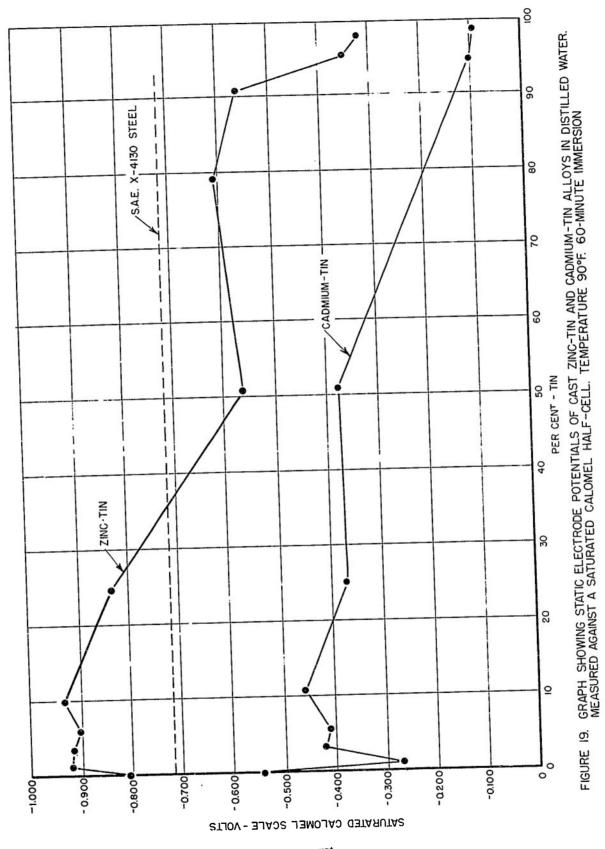
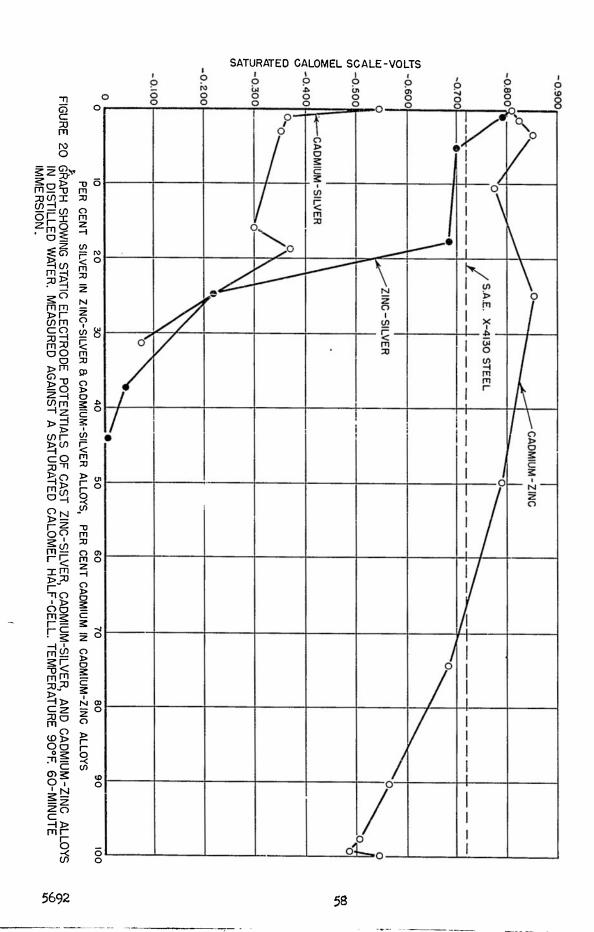


FIGURE 18. GRAPH SHOWING STATIC ELECTRODE POTENTIALS FOR CAST ZINC-COPPER ALLOYS IN DISTILLED WATER.
MEASURED AGAINST A SATURATED CALOMEL HALF-CELL. TEMPERATURE 90°F. 60-MINUTE IMMERSION





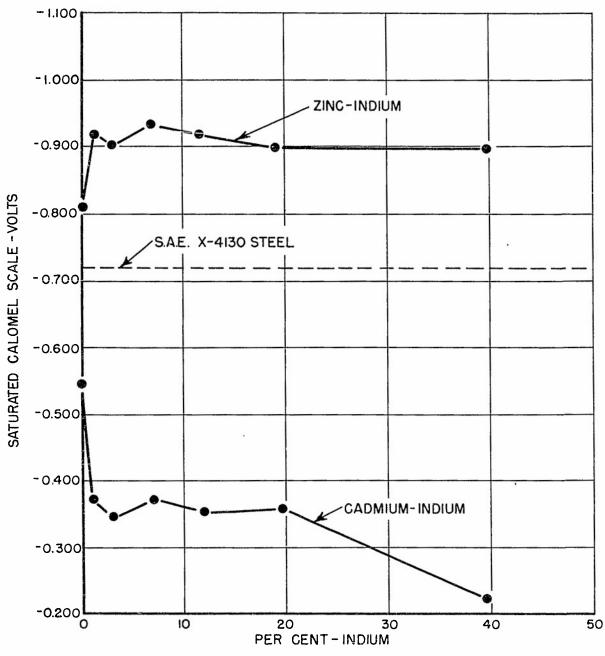


FIGURE 21. GRAPH SHOWING STATIC ELECTRODE POTENTIALS OF CAST ZINC-INDIUM AND CADMIUM-INDIUM ALLOYS IN DISTILLED WATER. MEASURED AGAINST A SATURATED CALOMEL HALF-CELL. TEMPERATURE 90°F. 60-MINUTE IMMERSION

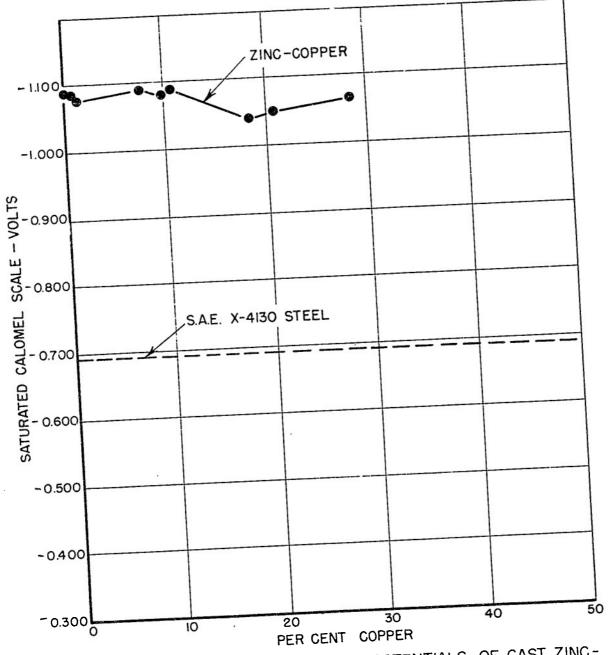
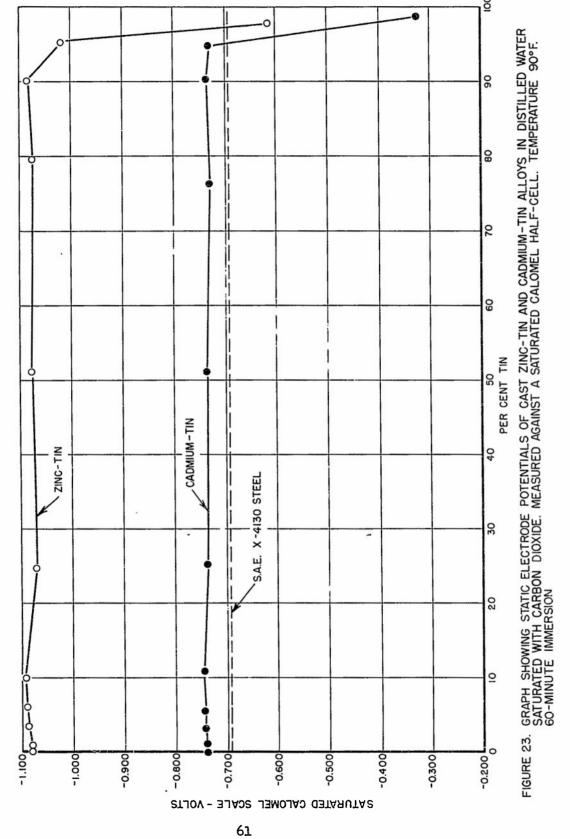
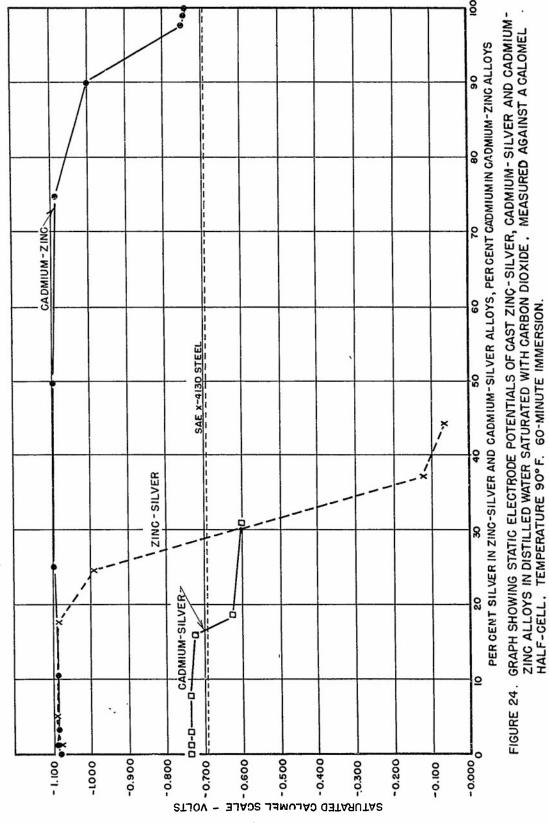


FIGURE 22. GRAPH SHOWING ELECTRODE POTENTIALS OF CAST ZINC-COPPER ALLOYS IN DISTILLED WATER SATURATED WITH CARBON DIOXIDE. TEMPERATURE 90°F. MEASURED AGAINST A SATURATED CALOMEL HALF-CELL. 60-MINUTE IMMERSION





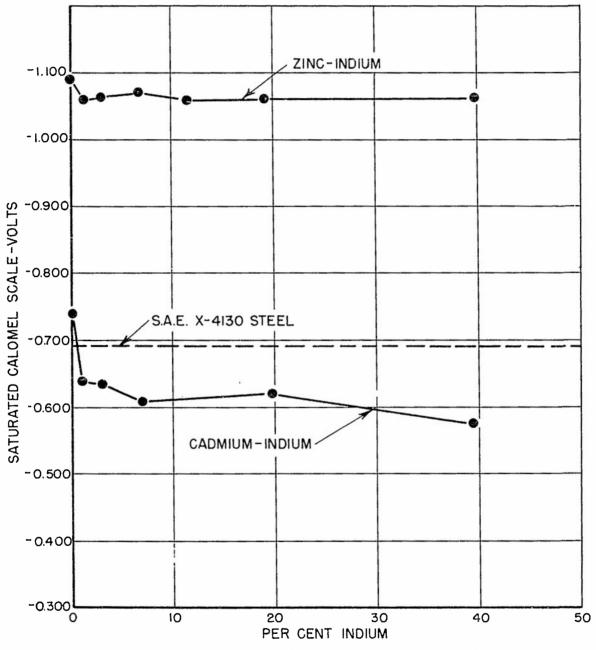


FIGURE 25. GRAPH SHOWING STATIC ELECTRODE POTENTIALS OF CAST ZINC-INDIUM AND CADMIUM-INDIUM ALLOYS IN DISTILLED WATER SATURATED WITH CARBON DIOXIDE. MEASURED AGAINST A SATURATED CALOMEL HALF-CELL. TEMPERATURE 90°F. 60-MINUTE IMMERSION

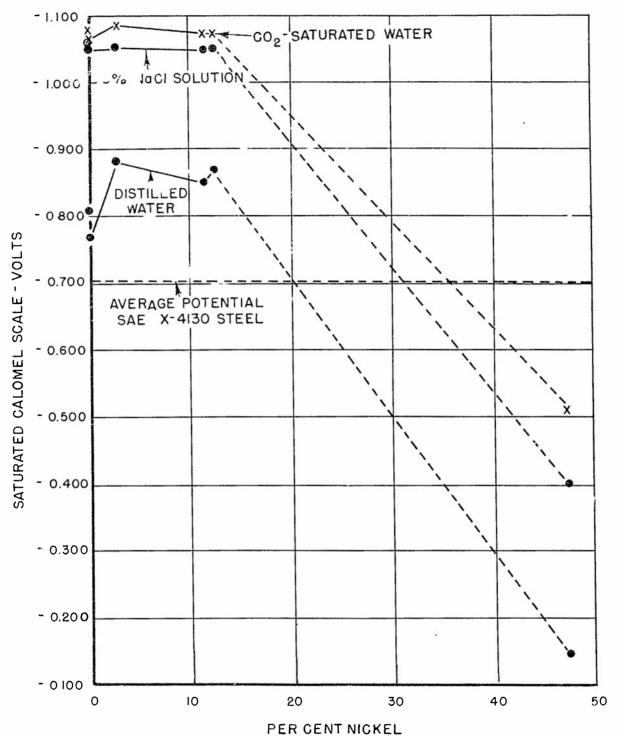


FIGURE 26 GRAPH SHOWING STATIC ELECTRODE POTENTIALS OF CAST ZINC-NICKEL ALLOYS IN 3% No CI SOLUTION, CO2-SATURATED WATER, AND DISTILLED WATER. MEASURED AGAINST A SATURATED CALOMEL HALF-CELL. TEMPERATURE 90° F. 60-MINUTE IMMERSION.

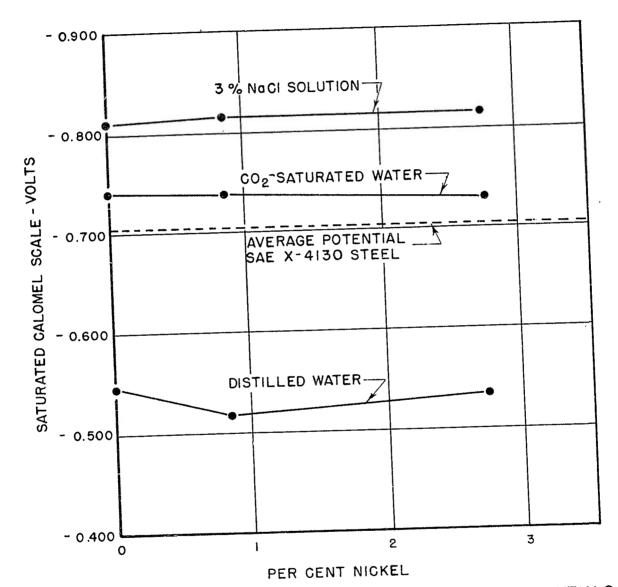


FIGURE 27. GRAPH SHOWING STATIC ELECTRODE POTENTIALS OF CAST CADMIUM-NICKEL ALLOYS IN 3% Na CI SOLUTION, CO₂-SATURATED WATER, AND DISTILLED WATER. MEASURED AGAINST A SATURATED CALOMEL HALF-CELL. TEMPERATURE 90°F. 60-MINUTE IMMERSION.

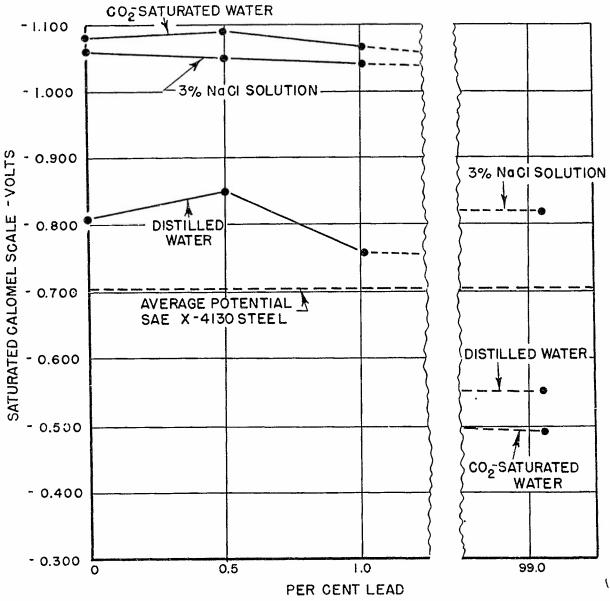


FIGURE 28. GRAPH SHOWING STATIC ELECTRODE POTENTIALS
OF CAST ZINC-LEAD ALLOYS IN 3% NaCI SOLUTION,
CO2-SATURATED WATER, AND DISTILLED WATER.
MEASURED AGAINST A SATURATED CALOMEL HALFCELL. TEMPERATURE 90° F. 60-MINUTE IMMERSION.

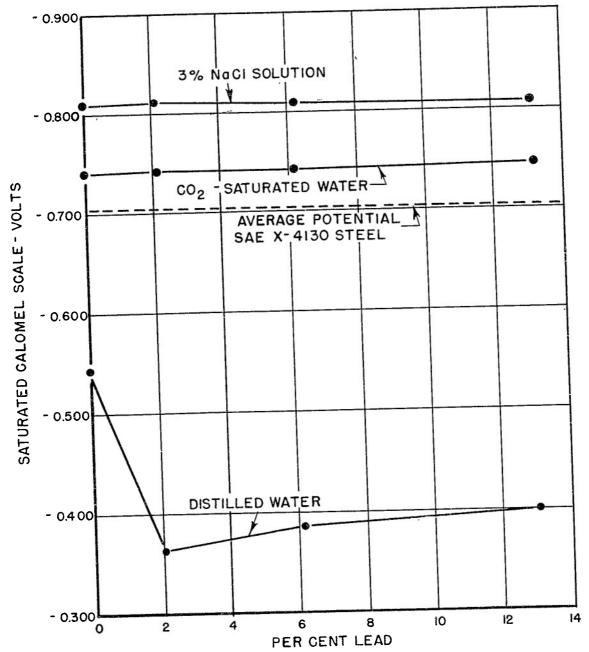


FIGURE 29. GRAPH SHOWING STATIC ELECTRODE POTENTIALS
OF CAST CADMIUM-LEAD ALLOYS IN 3% NaCI SOLUTION, CO2-SATURATED WATER, AND DISTILLED
WATER. MEASURED AGAINST A SATURATED CALOMEL
HALF-CELL. TEMPERATURE 90° F. 60-MINUTE
IMMERSION.

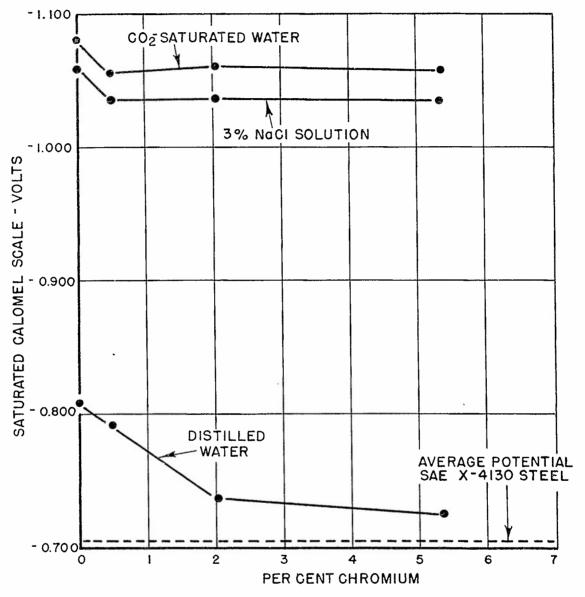


FIGURE 30. GRAPH SHOW STATIC ELECTRODE POTENTIALS OF CAST ZINC-CHROMIUM ALLOYS IN 3% NaCI SOLUTION, CO2-SATURATED WATER AND DISTILLED WATER. MEASURED AGAINST A SATURATED CALOMEL HALF-CELL. TEMPERATURE 90°F. 60-MINUTE IMMERSION

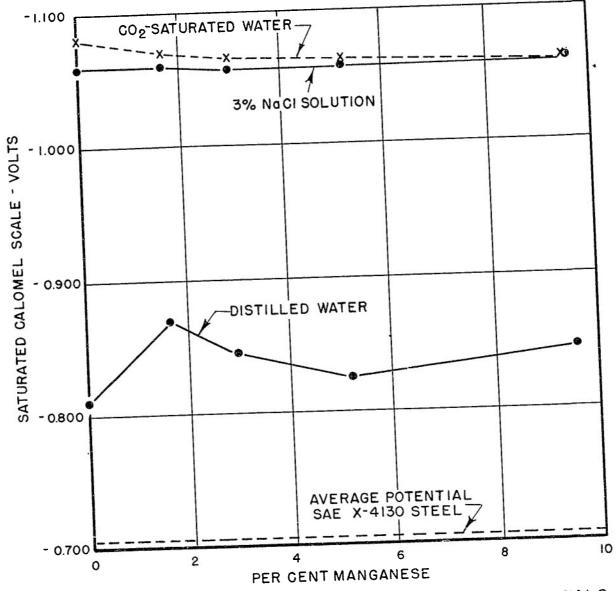
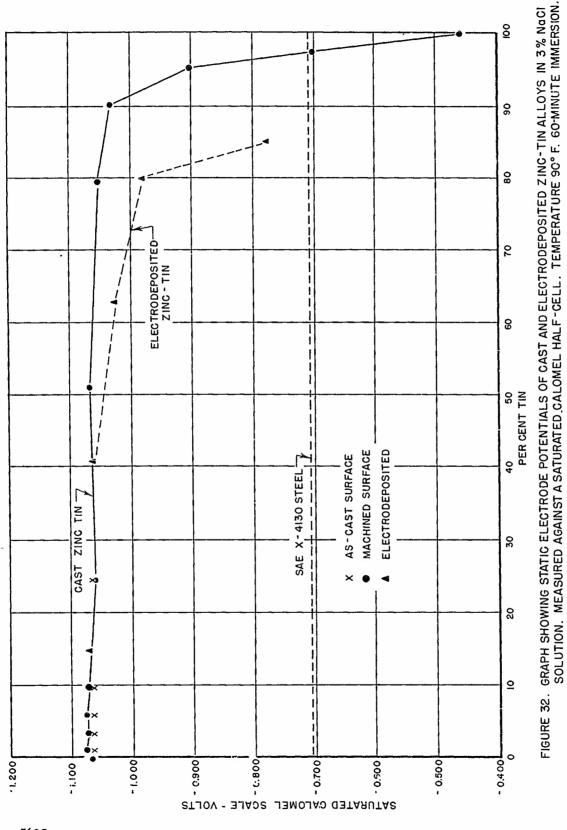
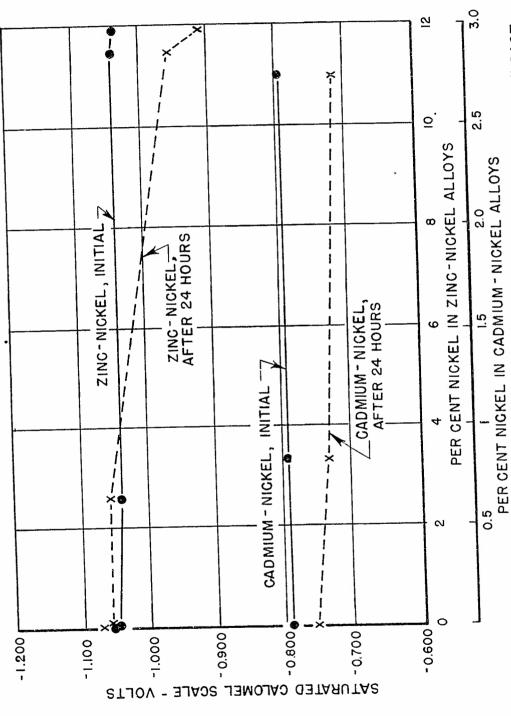


FIGURE 31. GRAPH SHOWING STATIC ELECTRODE POTENTIALS OF CAST ZINC-MANGANESE ALLOYS IN 3% NaCI SOLUTION, CO₂-SATURATED WATER AND DISTILLED WATER. MEASURED AGAINST A SATURATED CALOMEL HALF-CELL. TEMPERATURE 90° F. 60-MINUTE IMMERSION.



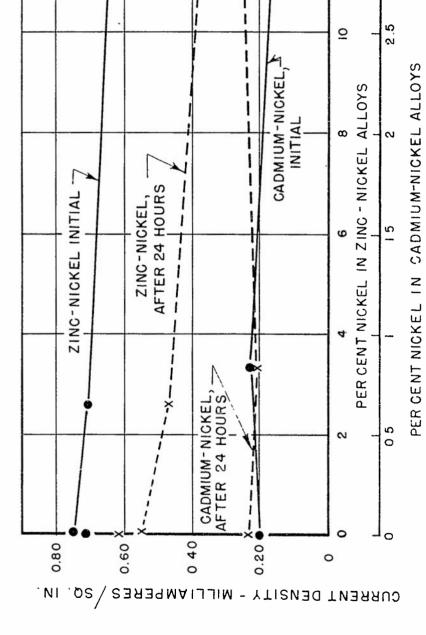


ZING-NIGKEL AND CADMIUM-NIGKEL ALLOYS COUPLED WITH STEEL IN 3% SODIUM CHLORIDE SOLUTION. MEASURED AGAINST A SATURATED CALOMEL HALF-GELL TEMPERATURE 90° F.

GRAPH SHOWING DYNAMIC ELECTRODE POTENTIALS OF CAST

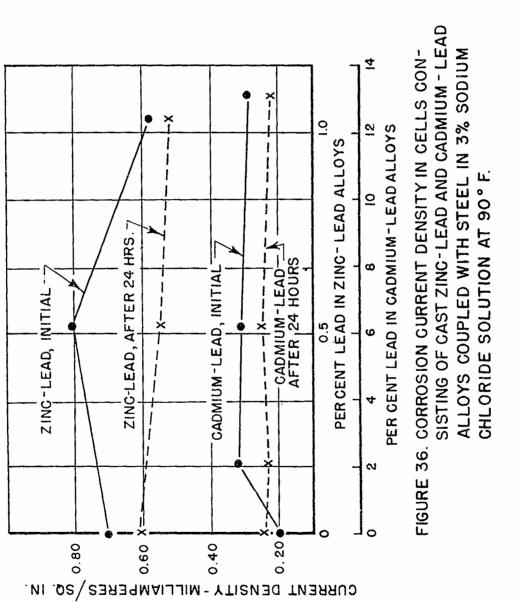
FIGURE 33.

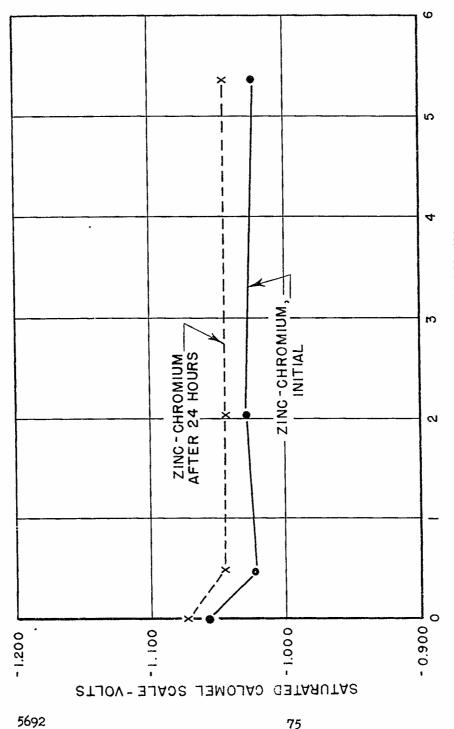
71



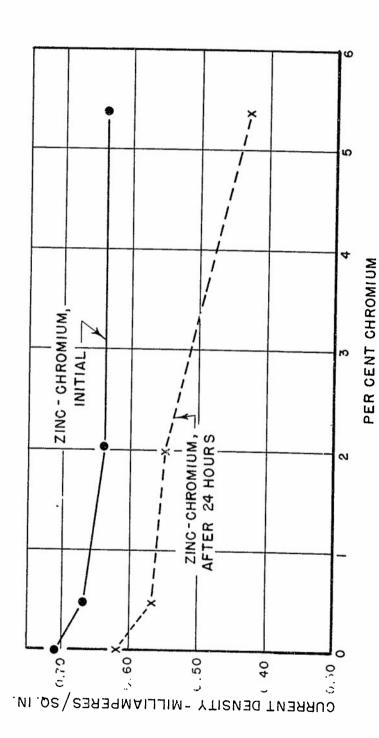
ZING - NICKEL AND CADMIUM - NICKEL ALLOYS COUPLED WITH CORROSION CURRENT DENSITY IN CELLS CONSISTING OF CAST STEEL, IN 3% SODIUM CHLORIDE SOLUTION AT 90° F. FIGURE 34

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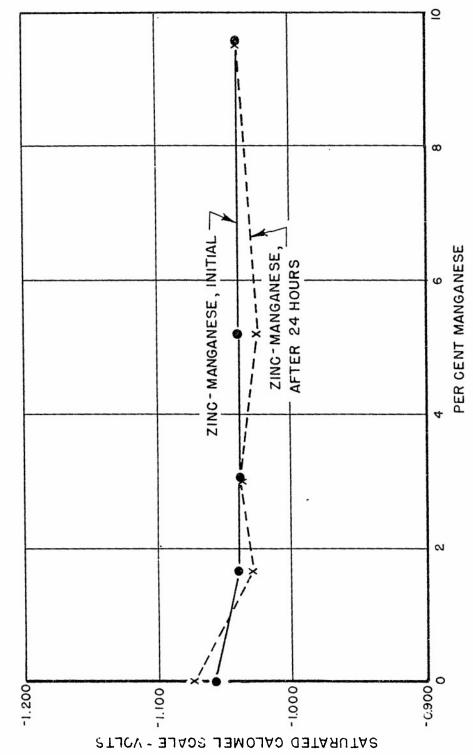


CHLORIDE SOLUTION. MEASURED AGAINST A SATURATED CALO-MEL HALF-CELL, TEMPERATURE 90° F. ZING-CHROMIUM ALLOYS COUPLED WITH STEEL IN 3% SODIUM FIGURE 37. GRAPH SHOWING DYNAMIC ELECTRODE POTENTIALS OF CAST PER CENT CHROMIUM



CORROSION CURRENT DENSITY IN CELLS CONSISTING OF CAST ZINC"-CHROMIUM ALLOYS COUPLED WITH STEEL, IN 3% SODIUM CHLORIDE SOLUTION AT 90°F. FIGURE 38.

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SOLUTION MEASURED AGAINST A SATURATED CALOMEL HALF- CELL, MANGANESE ALLOYS COUPLED WITH STEEL IN 3% SODIUM CHLORIDE FIGURE 39. GRAPH SHOWING DYNAMIC ELECTRODE POTENTIALS OF CAST ZING-TEMPERATURE 90°F

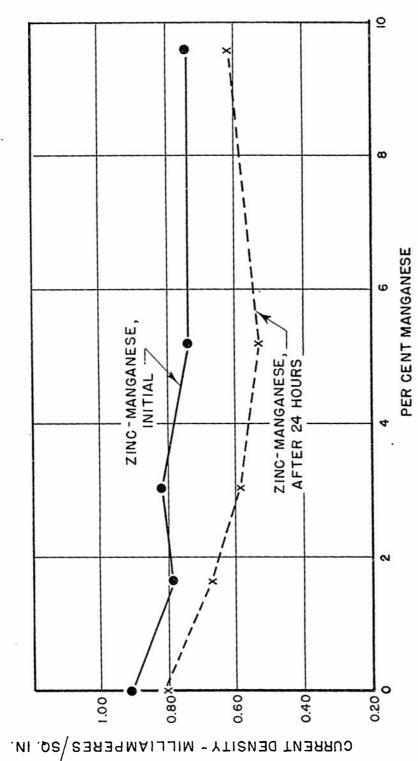


FIGURE 40. CORROSION CURRENT DENSITY IN CELLS CONSISTING OF CAST ZING-MANGANESE ALLOYS COUPLED WITH STEEL IN 3% SODIUM CHLORIDE SOLUTION AT 90° F.

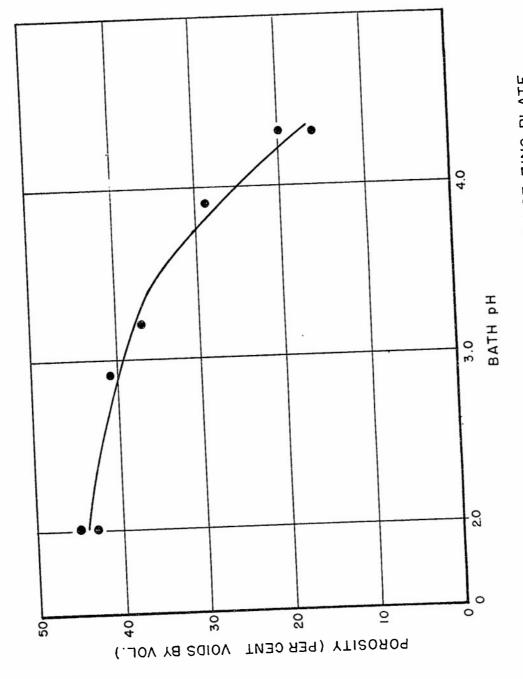


FIGURE 41. EFFECT OF PATH DH ON POROSITY OF ZING PLATE

APPENDIX III

This Appendix contains all data relative to potentials and corrosion current densities in tabulated form.

TABLE 1. POTENTIAL-TIME DATA FOR CAST ALLOYS BEFORE ANNEALING. THREE PER CENT NaCl SOLUTION, 90°F., SATURATED CALOMEL SCALE, VALUES IN VOLTS*

			Specim	en Numb	er and	Per Cent	Copper	
Elapsed Time	1-A	12-D	12-B	12-C	13-A	11-A	36 - B	38-B
(Min.)	0.74	1.22	7.56	9.62	10.5	18.34	20.75	28.4
	1 000	7 000	7 07/	1 000	7 000	0.000		
0	1.023	1.022	1.016	1.023	1.003	0.998	0.000	0.000
1 5 7							0.935	0.900
5							0.914	0.919
	1.027	1.031	1.026	1.027	1.005	1.002		
10							0.949	0.922
15	1.030	1.036	1.032	1.027	1.009	1.008		0.934
20							0.966	0.941
25	1.033	1.042	1.036	1.038	1.010	1.014	0.973	
30							0.979	0.950
35								0.954
40	1.039		1.042	1.043	1.013	1.019	0.984	0.955
50			330			•	0.991	0.958
55	1.045		1.046	1.042	1.019	1.024		
60			1.048				1.001	0.959
75			20040				1.018	~~//
90		1.056					4.040	
100		1.000			1.023			
					エ・リスク	1.021		
115						±•∪≈±	1 022	
150							1.033	
160							1.033	

^{*} All values are negative

TABLE 2. POTENTIAL-TIME DATA FOR CAST ALLOYS AFTER ANNEALING AT 400°C. ± 10°C. FOR 17 HOURS. THREE PER CENT NaCl SOLUTION, 90°F., SATURATED CALOMEL SCALE, VALUES IN VOLTS*

			Number and			
Elapsed Time (Min.)	1-A 0.74	12-D 1.22	12 - B 7 .5 6	12 - 0 9.62	13-A 10.5	11-A 18.34
				T		
1	1.030	1.021	1.026	1.026	1.013	0.876
5	1.034	1.031	1.033	1.026	1.021	0.956
10	1.037		1.037	1.028	1.024	0.975
15	1.038	1.041	1.039	1.033	1.026	0.983
20	1.040	1.044	1.041	1.035	1.027	0.988
25	1.041	1.047	1.044	1.037	1.028	0.992
30	1.042	1.050	1.045	1.038	1.030	0.995
35	1.043	1.052	1.046	1.039	1.030	0.996
40	1.044	1.053	1.047		1.030	0.998
45	1.045	1.055	1.047	1.041	1.031	1.000
50	1.046		1.047	1.042	1.031	1.001
55		1.057	1.048	1.042	1.031	1.002
60	1.048	1.059	1.048	1.043	1.031	1.003

^{*} All values are negative

POTENTIAL-TIME DATA FOR ELECTRODEPOSITED ALLOYS. THREE PER CENT NaCl SOLUTION, 90°F., SATURATED CALOMEL SCALE, VALUES IN VOLTS.* TABLE 3.

				10000	mr.W	Sacratimen Number and Per Cent Copper	Per Cen	t Coppe	Ą			
				opec	11011	1	0 70	30-B	38-A	8-A	₹-07	22-B
Elapsed Time	18-A	17-B	14-C	13-0 7.8	22-D 9.38	29-E 12.65	13.7	14.7	15.2	6	-	27.8
(W.T.W.)	1											
	5	1.011	1,013		0,999 0,980	0,980	0.985	0.997	0.970	0.985 0.997 0.970 1.032 0.907		906.0
→	7*O*T	100			0	199	686.0	1,014	0.987	1.039	0.928	916.0
ĸ	1.032	1.031	T.029	070.7	TOTAL TOTAL AZOT						ò	00.00
OL	1.038	1.037	1.034	1.024	1.034 1.024 1.006 0.998	866.0	0.998	1,021	0.990	1.044	0.94×	0.76.0
) ¥	1,040			1.026	1,008 0,999	0.999	1,001	1,021	686.0	1.046	0.957	0.928
ને ક						1.002	1.002	1,022		1.047	796*0	0.925
3 3					1.029 1.013	1.006	1,003		1.024 0.994	1,047		0.925
52	T*047					i (ָרָ ר		1,000	1,048	0.974	0.928
8	1.045		1.039	1.039 1.039 1.030	1.014	1.002	T•004					0
አራ	270-1	1,040		1.030	1.038 1.030 1.016	1,006			1.005			0.928
3 5	ά λ λ			1.030	1.016	1.016 1.007	1,008	1.025		1.047	0.982	0.928
O\$ 1	0,00					1.010	1.010		1.026 1.008		786.0	0.928
C7 ¹	1				1.019	1,011		1.028	1.028 , 1.013		986.0	0.925
S.	1.04%						1.015					0.925
55	1.050	1.045			1.04						6	0 005
9	1.050	1.047			1.024	1,024 1,013	1.017	1.017 1.030	1.016		0.700	11

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TABLE 4. POLARIZATION AND CORROSION CELL CURRENT DATA FOR CAST AND ELECTRODEPOSITED ALLOYS. THREE PER CENT NaCl, 90°F., SPECIMENS 1 INCH APART, 1-1/2-INCH IMMERSION. VOLTAGES ON SATURATED CALOMEL SCALE.

****		men Number and	l Per Cent Copp	
	12-B	13-C Electro-	38-B	22-B Electro-
	Cast 7.56	deposited 7.8	Cast 28.4	deposited 27.8
No Current Flowing				
l. X-4130 vs. calomel electrode	0.69 V.	0.68 V.	0.70 V.	0.675 V.
2. Alloy vs. calomel electrode	1.028 V.	1.01 V.	0.925 V.	0.92 V.
3. Calculated dif- ference between 1 and 2.	0.338 V.	0.33 V.	0.225 V.	0.245 V.
4. X-4130 vs. alloy (measured)	0.334 V.	0.325 V.	0.225 V.	0.25 V.
Cell Short-Circuited				
5. X-4130 vs. alloy	0.00 V.	0.00 V.	0.00 V.	0.00 V.
6. Current	2.2 ma.	2.2 ma.	1.1 ma.	1.1 ma.
7. Current density	0.63 ma./ sq.in.	0.7 ma./sq. in.	0.31 ma./sq. in.	0.35 ma./ sq.in.
8. X-4130 vs. calomel electrode	1.025 V.	1.01 V.	0.925 V.	0.92 V.
9. Alloy vs. calomel electrode	1.025 V.	1.01 V.	0.925 V.	0.92 V.

TABLE 5. POTENTIAL-TIME DATA FOR CAST ZINC-TIN ALLOYS IN 3% SODIUM CHLORIDE SOLUTION AT 90° F. SATURATED CALOMEL SCALE, VALUES IN VOLIS*

*** eu Wins	1,054	1.077	1.074	1.075	1.071	1,001	1.066	1.051		
V at Elapsed Time of:	55 MILES	1.076	1.074	1.073	1.070	3 1.060	3 1.065	7 1,051	1 0011.	
V at Ele	1 Min. 30 Mins.	1.045 1.049	1,053 1,073		1.055 1.065	1.045 1.056	1.063	770.1 7.047	L.O.	are negative with respect to the saturated card
	60 Mins. 1 h	7						1,067	1,051	pect to the sa
	<u>نا</u> .	- C	1,065	1,065	1,064	1,065	1,065	1,067	1,050	tive with res
	A	11	- J.062	1,062	1,058				1,051	₫ <u> </u>
		Specimen g Sn 1 Min.	0	53-A 1.08 1.054	3.44 L.S	10.9	0°5 86°6	24.7	51.1 L.	53-6 79.5 L.
		Specimen No.	50-B	53-A	53-B	53-C	53-D	53-E	53-F	53-0

* All the values given are negatare All the plotted in Figure 9.

TABLE 6. POTENTIAL-TIME DATA FOR CAST CADMIUM-TIN ALLOYS IN 3 PER CENT SODIUM CHLORIDE SOLUTION AT 90°F., SATURATED CALOMEL SCALE, VALUES IN VOLTS*

		V. at Elapse	d Time of: **	60 Mins.
% Sn	1 Min.	30 Mina.)) IIIII08	
0.0	0.793	0.805	0.808	0,•809
1.01	- 0.753	0.771	0.775	0.776
3 . 18	0.734	0.775	0.779	0.779
5.46	0.753	0.762	0.766	0.766
10.8	0.742	0.766	0.771	0.771
25.2	0.734	0.768	0.770	0.770
	0.725	0.766	0.762	0.762
76.2	0.743	0.729	0.728	0.728
	0.696	0.668	0.649	0.644
		0.461	0.459	0.460
		0.448	0.454	0.454
	0.0 1.01 3.18 5.46 10.8 25.2 51.1 76.2	0.0 0.793 1.01 0.753 3.18 0.734 5.46 0.753 10.8 0.742 25.2 0.734 51.1 0.725 76.2 0.743 90.2 0.696 94.9 0.693	% Sn 1 Min. 30 Mins. 0.0 0.793 0.805 1.01 0.753 0.771 3.18 0.734 0.775 5.46 0.753 0.762 10.8 0.742 0.766 25.2 0.734 0.768 51.1 0.725 0.766 76.2 0.743 0.729 90.2 0.696 0.668 94.9 0.693 0.461	0.0 0.793 0.805 0.808 1.01 0.753 0.771 0.775 3.18 0.734 0.775 0.779 5.46 0.753 0.762 0.766 10.8 0.742 0.766 0.771 25.2 0.734 0.768 0.770 51.1 0.725 0.766 0.762 76.2 0.743 0.729 0.728 90.2 0.696 0.668 0.649 94.9 0.693 0.461 0.459

^{*} All values are negative.

^{**} Values plotted in Figure 9.

TABLE 7. INITIAL AND 24-HOUR DYNAMIC POTENTIAL AND CORROSION CURRENT DATA FOR CAST ZINC-TIN AND CADMIUM-TIN ALLOYS COUPLED WITH STEEL. COUPLES IMMERSED IN 3 PERCENT SODIUM-CHLORIDE SOLUTION AT 90°F DURING MEASUREMENTS. SATURATED CALOMEL SCALE

		Initial !	Measurements	24 Hour-1	Measurements
Specimen No	% Sn	VGonvled	Corrosion Current Density in Na./In.2	VCoupled	Corrosion Current Den- sity in Ma./In.
Specimen No.		1111Oy	Picte/ Alle~	ALLOY	ARC. of LLILO
Zinc-Tin Seri 50-3	<u>es</u> 0∙00	1,056	0.63	1.069	0.735
53 - A	1.03	1.07	0.874	1.075	0.772
53 - B	3.44	1.08	0.766	1.075	0.671
53 - C	6.01	1.07	0.732	1.075	0.707
53 - D	9.98	1.07	0.772	1.075	0.733
53-E	24.7	1.07	0.737	1.075	0.598
53 - F	51.1	1.05	0.758	1.045	0,48
53 - 0	79.5	1.05	0.707	0.99	0.366
Cadmium-Tin S	Series 0.00	0.784	0.20	0.752	0.23
55 - A	1.01	0.775	0.19	0.768	0.178
55 - B	3.18	0.763	0.148	0.766	0.197
55 - C	5.46	0.773	0.185	0.759	0.197
55 - D	10.8	0.771	0.20	0.776	0.20
55 - I	25•2	0.759	0.172	0.757	0.224
55 - F	51.1	0.755	0.178	0.741	0.216
55 - G	76.2	0.734	0.132	0.682	0.185
55-H	90.2	0.705	0.049	0,677	*

^{*}Steel corroded. Wo measurement possible.

TABLE 8. POTENTIAL-TIME DATA FOR CAST ZINC-SILVER AND CADMIUM-SILVER ALLOYS IN 3 PER CENT SODIUM CHLORIDE SOLUTION AT 90°F., SATURATED CALOMEL SCALE, VALUES IN VOLTS*

			Volts at Elaps	sed Time of:	,
Specimen No.	% Ag	1 Min.	30 Mins.	50 Mins.	60 Mins
		(Zinc-Silve	System)		
287562-A-1	1.02	1.030	1.045	1.047	1.049
62-B-1	5.14	1.025	1.040	1.042	1.01,3
62-C-l	17.8	1.019	1.032	1.035	1.035
62-0-1	24.8	0.945	0.925	0.924	0.924
62-E-1	37.2	0.416	0.267	0.281	0.279
62-F-1	1,1,2	0.332	0.227	0.218	0.217
		(Cadmium-Sil	ver System)		
287560-A-1	1.24	0.803	0.800	0.800	0.800
60-B1	3.04	0.805	0.810	0.807	0.806
60-c-l	7.95	0.808	0.809	0.806	0.804
-60-D-1	16.0	0.789	0.795	0.769	0.759
-60-E-2	18.65	0.758	0.679	0.705	0.708
60-F-1	31.2	0.724	0.571	0.539	0.523

^{*} All values are negative.

^{**} Values plotted in Figure 7.

TABLE 9. POTENTIAL-TIME DATA FOR CAST CADMIUM-ZINC ALLOYS IN 3 PER CENT SODIUM CHLORIDE SCLUTICN AT 90°F., SATURATED CALOMEL SCALE, VALUES IN VOLTS**

			Volts at Elap	sed Time of:	
Specimen No.	% Zn	1 Min.	30 Mins.	50 Mins.	60 Mins.
2875—57-A-1	0.91	0.740	0.737	0.739	0.740
-57-B-1	2.35	0.816	0.728	0.730	0.733
-57-C-1	9.83	0.993	0.988	0.991	0.982
-57-D-1	25.6	1.033	1.042	1.041	1.040
-57-E-1	50,2	1.01;7	1.062	1.062	1.058
-57-F-1	7)4.9	1.050	1.063	1.065	1.063
-57-G-1	89.5	1.050	1.062	1.063	1.062
-57-H-1	96.7	1.050	1.063	1.066	1.066
-57-I-1 -57-I-1	98.7	1.053	1.070	1.067	1.069

^{*} All values are negative.

^{**} Values plotted in Figure 7.

TABLE 10. POTENTIAL-TIME DATA FOR CAST ZINC-INDIUM AND CADMUM-INDIUM ALLOYS IN 3 PER CENT SODIUM CHLORIDE SOLUTION AT 90°F., SATURATED CALOMEL SCALE, VALUES IN VOLTS*

					į.
Specimen No. %	In	l Min.	Volts at Elaps 30 Mins.	sed Time of: 50 Mins.	60 Mins.
		(Zinc-Indium	System)	יי סטל	1.077
2875—71-A-1	1.2	1.056	1.072	1.075	1.072
-71-B-1	3.0	1.057	1.068	1.073	1.074
-71-C-1	6.8	1.051	1.069	1.071	1.071
71-D-1	11.5	1.049	1.067	1.062	1.064
71-E-1	19.0	1.045	1.062	1.064	1.063
71-F-1	39.6	1.052	7.000		
		(Cadmium-Ir	ndium System)		
	1.1	0.726	0.735	0.736	0.737
2875—70-A-1	3.0	0.720	0.717	0.718	0.718
70-B-1	7.0	0.711	0.714	0.716	0.717
70-C-1	11.9	0.715	0.718	0.720	0.720 0.715
- 70-D-1 70-E-1	19.7	0.717	0.713	0.714	0.713
- 70-F-1		0.718	0.708	0.712	

^{*} All values are negative.

^{**} Values for 60 minutes plotted in Figure 8.

TABLE 11. POTENTIAL-TIME DATA FOR SOME ADDITIONAL ZINC-TIN ALLOYS IN 3 PER CENT SOFTUM CHLORIDE SOLUTION AT 90°F., SATURATED CALOMEL SCALE, VALUES IN VOLTS*

			Volts at El	apsed Time of	•
Specimen No.	% Sn	l: Min.	30 Mins.	50 Mins.	60 Mins*
2875—87-A-1	90.13	1.032	1.018	1.011	1.008
87-B-1	95.30	0.902	0.664	0.641	0.631
-87-C-1	97.80	0.700	0.599	0.591	0.588
l .					

^{*} All values are negative.

^{***} Sixty-minute values plotted in Figure 9.

PABLE 1:. INITIAL AND 24-HOUR DYNAMIC POTENTIAL AND CORROSION CURRENT DATA FOR CAST ZINC-SILVER AND CADMIUM-SILVER ALLOYS COUPLED WITH STEEL. COUPLES IMMERSED IN 3 PER CENT NaCl at 90 F. FCR THE 24-HOUR PERIOD SATURATED CALOMEL SCALE.

			Vac aurements	24-Hour	Measurements
Specimen	% Ag	Coupled Alloy (Volts)	Corrosion Current Density (Ma./In.2)	Coupled Alloy (Volts)	Corrosion Current Density (Ma./In.2)
		(Zinc-S	Silver System)	
287562-A-1	1.02	1.038	0.76	1.063	0.82
	5.14	1.036	0.75	1.049	0.57
62-B-1	-	1.027	0.72	0.976	0.45
62-C-l		0.865	0.36	0.916	0.26
62-D-1			عند عند	*	*
62-E-J		*	*	*	*
62-F-	tem)				
			um-Silver Sys	0.717	0.26
287560-A-			0.25	0.736	0.17
60 -B -		-		0.723	0.20
60-C				*	*
60-D			*	*	*
60-E	-2 18.	.65 *	-	*	*
60-F	-1 31	.2 *	*		

^{*} Alloy was more noble than steel. No dynamic measurements were made.

TABLE 13. INITIAL AND 24-HOUR DYNAMIC POTENTIAL AND CORRESION CURRENT DATA FOR CAST CADMIUM-ZINC ALLOYS AND THREE ADDITIONAL ZINC-TIN ALLOYS COUPLED WITH STEEL. COUPLES IMMERSED IN 3 PER CENT NAC1 at 90°F. FOR THE 24-HOUR PERIOD. SATURATED CALOMEL SCALE

		Initial	Measurements	24-Hour	Measurements	
			Corrosion		Corrosion	
_		Coupled	Current	Coupled	Current	
Specimen		Alloy	Density	Alloy	Density	
No.	% Cd	(Volts)	(Ma./In. ²)	(Volts)	(Ma./In. ²)	
		(Cadmix	m-Zinc System	.)		
87557-A-1	99.09	0.745	0.11	0.781	0.26	
57-B-1	97.65	0.757	0.16	0.751	0.23	
57-C-l	90.17	1.007	0.50	0.736	0.17	
57-D-1	74.4	1.036	0.66	0.976	0.36	
57-E-1	49.8	1.052	0,79	1.029	0.51	
57-F-1	25.1	1.060	0.70	1.058	0.57	
-57-G-1	10.5	1.059	0.74	1.062	0.63	
— 57-H-1	3.3	1.061	0.77	1.056	0.63	
57-I-1	1.3	1.067	0.83	1.073	0.61	
(Zinc-Tin System)						
	% Sn					
2875-87-A-1	90.13	1.016	0.57	0.745	0.18	
87-B-1	95.3	0.761	0.18	0.689	*	
87-C-1	97.8	*	*	*	*	

^{*} Alloy was more noble than steel. No dynamic measurements were made.

TABLE 14. INITIAL AND 24-HOUR DYNAMIC POTENTIAL AND CORROSION CURRENT DATA FOR CAST ZINC-INDIUM AND CADMIUM-INDIUM ALLOYS COUPLED WITH STLEL. COUPLES IMMERSED IN 3 PER CENT NaCl AT 90°F. FOR THE 24-HOUR PERIOD. SATURATED CALOMEL SCALE.

		Initial	Measurements	24-Hour	Measurements	
		Coupled	Corrosion Current	(lana 1 - 3	Corrosion Current	
Specimen		Alloy	Density	Coupled Alloy	Density	
No.	% In	(Volts)	(Ma./In.2)	(Volts)	(Ma./In.2)	
740.0	- C	(10108)	(1121) 2110	(46.68)	(1130.0 / 111.0 /	
(Zino-Indium System)						
2875-71-A-1	1.2	1.055	0.88	1.073	0.91	
71-B-L	3.0	1.056	0.83	1.076	0.66	
71-C-I	6.8	1.059	0.80	1.078	0.82	
71-D-1	11.5	1.054	0.80	1.075	0.72	
71-E-1	19.0	1.051	0.86	1.074	0.C9	
71F-1	39.6	1.048	0.83	1.061	0.61	
(Cadmium-Indium System)						
2875-70-A-1	1.1	0.721	0.043	0.730	0.17	
70-B-1	3.0	0.720	0.086	0.732	0.23	
70-C-1	7.0	0.722	0.043	0.728	0.27	
70-u-1	11.9	0.724	0.043	0.727	0.14	
70-E-1	19.7	0.723	0.057	0.726	0.19	
70-F-1	39.5	0.7.19	0.029	0.715	0.12	
	70. 9	J#1.20	0,000	7,120	0.10	

TABLE 15. POTENTIAL-TIME DATA FOR CAST ZINC-COPPER ALLOYS IN DISTILLED MATER AT 90°F., SATURATED CALOMEL SCALE, VALUES IN VOLTS*

Specimen			Volts at Elapsed Time of:			
No.	% Cu	60 Mins#*	75 Mins.	90 Mins.		
2875—1-A	0.74	0.833	0.835	0.830		
12-D	1.22	0.866	0.875	0.880		
12-B	7.56	0.805	0.7 99	0.806		
12-0	9.62	0.839	0.860	0.880		
13-A	10.5	0.800	0.765	0.763		
11-A	18.34	0.685	0.685	0.715		
36- B	20.75	0.464	0.491	0.537		
38 −B	28.4	0.311	0.249	0.255		
			• • •			

^{*} All values are negative.

^{**} Sixty-minute velues are plotted in Figure 18.

TASLE 16. POTENTIAL-TIME DATA FOR CAST ZÎNC-TIN ALLOYS ÎN DISTILLED WATER AT 90°F., SATURATED CALCWEL SCALE, VALUES ÎN VOLTS*

Specimen	pecimen Volts at Elapsed; Time of i				
No.	% Sn	60 Mins. **	75 M ins.	90 Mins.	
287553-A-l	108	0.919	0.910	0.90 0	
53-B1	3.44	0.915	0.936	0.937	
53-C-J.	6.01	0.903	0.947	0.947	
53-D-1	9.98	0.933	0.951	0.985	
53-E-1	24.7	೧_832	C.872	0.877	
53-F-1	51.1	0.565	0.578	0.575	
—53-G-√	79.5	0.610	0.633	0.642	
87-A-J	90.13	0.562	0.590	0.675	
87-3-1	95 .3	0.385	0.360	0.352	
87C-1	97.8	0.332	0.329	0.322	

^{*} All values are negative.

^{**} Sixty-minute values plotted in Figure 19.

TABLE 17. POTENTIAL-TIME DATA FOR CAST CADMIUM-TIN ALLOYS IN DISTILLED WATER AT 90°F, SATURATED CALOMEL SCALE, VALUES IN VOLTS*

Specimen		Volts at Elapsed Time of:			
No.	% Sn	60 Mins.**	75 Mins.	90 Mins	
287550-A	0.00	0.545	0.505	0.450	
55-A-1	1.01	0,268	0.286	0.301	
55-B-1	3.18	0.423	0.407	0.407	
55-C-1	5.46	0.412	0.426	0.436	
55-D-1	10.8	0.459	0.446	0.456	
55-E-1	25.2	0.371	0.367	0.364	
55-F-1	51.1	0.377	0.350	0.355	
55-G-1	76.2	••••		0.288	
55-H-1	90.2		****	0.294	
55-I-1	94•9	0.103	0.105	0.108	
55-J-2	98.8	0.095	0.130	0.165	

^{*} All values are negative.

^{**} Sixty-minute values are plotted in Figure 19.

TABLE 18. POTENTIAL-TIME DATA FOR CAST ZING-SILVER AND CADMIUM-SILVER ALLOYS IN DISTILLED WATER AT 90°F., SATURATED CALOMEL SCALE, VALUES IN VOLTS*

Specimen Volts at Elapsed Time of:										
No.	% Ag	60 Mins.**	75 Mins.	90 Mins.						
(Zinc-Silver System)										
2875	1,02	0.793	0.810	0.825						
62-B-1	5.14	0.700	0.822	0.808						
62-C-1	17.8	0,685	0.746	0.680						
62-D-1	24.8	0.220	0.227	0.230						
62-E-1	37.2	0.043	0.046	0.040						
62-F-1	44.2	0.008	0.005	0.000						
	(Cadı	nium-Silver Sys	stem)							
28 75 60-A-1	1.24	0.365	0.371	0.364						
60-B-1	3.04	0.383	0.375	0.384						
60-C-1	7.95	0.355	0.335	0.339						
60-D-1	16.0	0.300	0.276	0.302						
60-E-2	18.65	0.373	0.358	0.355						
60-F-1	31.2	0.072	0.065	0.065						

^{*} All values are negative.

^{**} Values for 60 mins. plotted in Figure 20.

TABLE 19. POTENTIAL-TIME DATA FOR CAST CADMIUM-ZINC ALLOYS IN DISTILLED WATER AT 90°F., SATURATED CALOMEL SCALE, VALUES IN VOLTS. *

Specimen		Volts at	Elapsed Ti	me of:
No.	% Cd	60 Mins. **	75 Mins.	90 Mins.
287557-4-1	99.09	0.454	0.476	0.485
57-B-1	97.65	0.465	0.491	0.504
57-0-1	90.17	0.544	0.549	0.565
57-D-1	74.4	0.673	0.682	0.684
57-E-1	49.8	0.792	0.785	0.790
57-F-1	25.1	0.847	0.854	0.855
57-G-1	10.5	0.785	0.784	0.778
57-H-l	3.3	0.832	0.837	0.847
57-I-1	1.3	0.808	0.813	0.825

All values are negative.

^{**} Values for 60 mins. plotted in Fig. 20.

TABLE 20. POTENTIAL-TIME DATA FOR CAST ZINC-INDIUM AND CADMIUM-INDIUM ALLOYS IN DISTILLED WATER AT 90 F., SATURATED CALOMEL SCALE, VALUES IN VOLTS *

Specimen				psed Time of:			
No.	%	In 60	Mins.** 75	Mins. 90 Mins			
(Zinc-Indium System)							
287571-A-1	1.2	ე.918	0.931	0.910			
71-B-1	3.0	0.900	0.888	0.378			
71-C-1	6.8	0.932	0.933	0.941			
71-D-1	11.5	0.917	0.914	0.915			
71-E-1	19.0	0.898	0.935	0.922			
71-F-1	39. 0	0.895	0.889	0.882			
	(Cadr	nium-Indium	System)				
287570-A-1	1.1	0.372	0.382	0.389			
70-B-1	3.0	0.347	0.368	0.373			
70-C-1	7.0	0.373	0.398	0.408			
70-D-1	11.9	0.353	0.858	0.362			
70-E-1	19.7	0.358	0.365	0.396			
//-F-1	39.5	0.224	0.240	0.237			

^{*} All values are negative.

^{**} Values for 60 mins. plotted in Fig. 21.

TABLE 21. POTENTIAL-TIME DATA FOR CAST ZINC-COPPER ALLOYS, MEASURED AT 90°F IN DISTILLED WATER SATURATED WITH CARBON DIOXIDE, SATURATED CALOMEL SCALE, VALUES IN VOLTS*

			Volts at Ele	apsed Time of	•
Specimen No.	% Cu	l Min.	30 Mins.	50 Mins.	60 Minė*
2875—1-A	0.74	1.077	1.083	1.085	1.085
12-D	1.22	1.074	1.075	1.077	1.078
12-B	7.56	1.076	1.088	1.088	1.090
-12-0	9.62	3.072	1.083	1.083	1.002
13-A	10.5	1.083	1.088	1.086	1.087
13-A	18.34	0.920	1.029	1.037	1.039
-36-E	20.75	1.035	1.047	1.047	1.048
3S-B	28.4	1.035	1.069	1.067	1.065

^{*} All values are negative.

Sixty-minute values plotted in Figure 22.

TABLE 22. POTENTIAL-TIME DATA FOR ZINC-TIN ALLOYS, MEASURED AT 90°F. IN DISTILLED WATER SATURATED WITH CARBON DIOXIDE, SATURATED CALONEL SCALE, VALUES IN VOLTS*

			Volts at Elap	osed Time of:	
Specimen No.	% Sn	1 Min.	30 Mins.	50 Mins.	60 Minšt
2875 53 - A-1	308	1.060	1.071.	1.077	1.080
53-B-1	3.44	1.061	1.076	1.084	1.086
- 53-C-1	6.01	1.063	1.083	1.089	1.091
53-D-1	9.98	1.068	1.091	1.093	1.093
53-E-1	24.7	1.050	1.063		1.070
53-F-1	51.1	1.056	1.069	, 	1.078
53-G-1	79•5	1.064	1.071;	. -	1.076
87-A-I	90.13	1.069	1,082	1.085	1.084
- S7-B-1	95•3	1.061	1.061	1.046	1.019
- 87-C-1	97.8	1.059	0.686	0.616	0.616

^{*} All values are negative.

^{**} Values at 60 minutes plotted in Figure 23.

TABLE 23. POTENTIAL-TIME DATA FOR CADMIUM-TIN ALLOYS, AT 90°F., IN DISTILLED WATER SATURATED WITH CAPEON DIOXIDE, SATURATED CALOMEL SCALE, VALUES IN VOLTS*

			Volts at Ela	apsed Time of:	
Specimen No.	% Sn	l Min.	30 Mins.	50 Mins.	60 Hirs
287555-A-1	1.01	0.708	0.733	0.739	0.740
-55-B-1	3.18	0.714	0.739	0.743	0.743
- 55-0-1	5.46	0.708	0.739	0.742	0.71;3
- 55-D-1	8.0.5	0.716	0.741	0.744	0.7/14
55-E-1	25.2	0.711	0.734	0.737	0.738
55-F-1	. 51.1	0.703	0.728	0.735	0.736
55-G-1	76.2	0.695	0.724	0.729	0.729
— 55-н-1	90•2	0.709	0.738	0.738	0.737
- 55-1-1	94.9	0.711	0.731	0.731	0.729
 55-, 1 -2	98.8	0.700	0.571	0.396	0,324

^{*} All values are negative.

^{**} Sixty-minute values are plotted in Figure 23.

TABLE 24. PCTENTIAL-TIME DATA FOR CAST ZINC-SILVER AND CADMIUM-SILVER ALLOYS, MEASURED AT 90°F. IN DISTILLED WATER SATURATED WITH CARBON DIOXIDE, SATURATED CALOMEL SCALE, VALUES IN VOLTS*

			Volts at Ela	apsed Time of	:
Specimen No.	% Ag	l Min.	30 Mins.	50 Mins.	60 Wins.
		(Zinc-Silve	r System)		
2 87562-1	1.02	1.066	1.082	1.082	1.082
- 62-B-1	5.14	1.060	1.084	1.090	1.091
-62-0-1	17.8	1.074	1.085	1.088	1.089
62-D-1	214.3	1.052	1.054	1.021	C.294
62-E-1	37.2	0.996	0.139	0.119	0.123
62-F-1	44.2	0.882	0.064	0.062	0.062
		(Cadmium-Si	lver System)		
2875-60-A-1	1.24	0.711	0.736	0.739	0.740
60-B-1	3.04	0.706	0.734	0.75?	0.737
-60-C-1	7.95	0.702	0.731	0.740	0.741
60-1	16.0	0.709	0.721	0.726	0.726
60-E-S	18.65	0.661	- 0.625	0.622	0.618
60-F-1	31.2	0.631	0.611	C*60H	0.603

^{*} All values are negative.

^{**} Values for 60 minutes are plotted in Figure 24.

TABLE 25. POTENTIAL-TIME DATA FOR CAST CADMIUM-ZING ALLCYS, MEASURED AT 90°F. IN DISTILLED WATER SATURATED WITH CARBON DIOXIDE, SATURATED CALOMEL SCALE, VALUES IN VOLTS*

			Volts at Ele	apsed Time of	:
Specimen No.	% Ců	1 Min.	30 Mins.	50 Mins.	60 Mins
2875-57-A-1	99.09	1.015	ver ess	0.745	0.745
57-F-1	97.65	1.045	0.797	0.758	0.755
57-3-1	90,17	1.063	1.059	1.018	0.999
- 57-D-1	74.4	1.066	1.089	1.088	1.087
57-E-1	49.8	1.063	1.088	1.092	1.092
57-F-1	25.1	1.072	1.090	1.095	1.095
-57-G-1	10.5	1.061	1.084	1.088	1.088
- 57-н-1	3.3	1.061	1.081	1.087	1.088
-57-I-1	1.3	1.064	1.085	1.089	1.089

^{*} All values are negative.

^{**} Valuer for 60 minutes plotted in Figure 24.

TABLE 26. POTENTIAL-TIME DATA FOR CAST ZINC-INDIUM AND CADMIUM-INDIUM ALLOYS, MEASURED AT 90°F. IN DISTILLED WATER SATURATED WITH CARBON DIOXIDE, SATURATED CALOMEL SCALE, VALUES IN VOLTS*

			Volts at Ela	apsed Time of	:
Specimen No.	Д In	l Min.	30 Mins.	50 Mins.	60 mins.
		(Zinc-India	ım System)		
2875—71-A-1	1.2	1.058	1.085	1.091	1.093
71-B-1	3.0	1.064	1.085	1,090	1.091
71-c-1	ñ.8	1.069	1.085	1.089	1.090
72-D-1	13.5	1.058	1.078	1.036	1.008
71-8-1	19.0	1.061	1.084	1.092	1.093
71-F-1	39.6	1.062	1.095	1.098	1.098
		(Cadmium-In	dium System)	•	
2875— 70-A-1	1.1	0.638	0.667	0.684	0.692
-70-B-1	3.0	0.634	0.659	0.677	ი.683
- 70-c-1	7.0	0.610	0.641	0.654	0.060
-70-D-1	11.9	0.610	0.646	C.654	0.660
70-E-1	19.7	0.620	0.640	0.651	0.656
70-F-1	39•5	0.578	0.573	0.581	0.589
L					

^{*} All values are negative.

^{**} Values for 60 minutes plotted in Figure 25.

TABLE 27. POTENTIAL-TIME DATA FOR CAST PURE METALS AND SAE X-4130 STEEL IN 3 PER CENT SODIUM CHLORIDE SOLUTION AT 90°F., SATURATED CALOMEL SCALE, VALUES IN VOLTS

	Specimen		Volts a	t Elapsed		
Motal.	No.	1 Min.	30 Mins.	50 Mins.	60 Mins.	160 Mins
Zinc	28 7550-B	-1.048	-1.056	-1.060	-1.061	****
Zinc	50-В	-1.045	-1.050	-	-1.055	
Zinc	88-A	-1.039	-1.059	-1.062	-1.064	
Gudmium	50-A	-0.793	-0.805	-0.808	-0.809	*****
Tin	73-B-J	-0.631	-0.458	-0.458	-0.457	******
Indium	73-A	-0.721	-0.678	-0.685	-0.687	****
litanium	3180—37-A	-0.373	-0.084	-0.006	+0.023	+0.09]
Zirconiu	—37-В	-0.210	+0.020	+0.083	+0.095	+0.140
Manganese	37-C	-1.390	-1.317	-1.315	-1.316	-1.30
X-4130 steel	2675-33-A	-0.617	-0.713	-0.711	-0.711	*****
Ditto	33-B	-0.619	-0.709	-0,708	-0,707	*****
11 .	72-A	-0.609	-0.701	-0.698	-0.697	-0.70
11	—72-В	-0.590	-0.710	-0,707	-0.707	-0.70

TABLE 28. POTENTIAL-TIME DATA FOR PURE METALS, MEASURED AT 90°F, IN DISTILLED WATER AND CARBON DIOXIDE SATURATED WATER, SATURATED CALOMEL SCALE, VALUES IN VOLTS*

	Specimen				sed Time	فالمستحدث ببينا ببينا ببينا ببنا	
Metal	No.	l Min.	30 Mins.	50 Mins.	60 Mins.	75 Mins.	90 Mins.
			(Distille	d Water)			
Zine	3180-5-**				১.809	0.865	0.873
Cadmium	2875-50-A				0.545	0.505	0.459
Y-4130 steel	28799-A	•			0.718	0.719	0.712
X-1130 steel	2875-99-B				0.718	0.720	0.721
	(Disti)	led Water	r Saturated	With Carb	on Dioxide)	
Zinc	2875-50-B	1.070	1.076		1.079	·	
Cadmium	2875-50-A	0.724	9.739	0.740	0.741		
X-4130 steel	3180-18-A	0.510	0.677	0.686	0.690		0.695
X-4130 steel	3180-18 - B	0.630	0.683	0.691	0.693		0.698

^{*} All values are negative.

^{**} Unmachined.

TABLE 29. POTENTIAL-TIME DATA FOR CAST ZINC AND CADMIUM SPECIMENS TREATED WITH THE CRONAK OR IRIDITE PROCESSES, IN 3 PER CENT SODIUM CHLORIDE SOLUTION AT 90°F., SATURATED CALOMEL SCALE, VALUES IN VOLTS

/h	Volts at Elapsed Time of:					of:		
Specimen No.	Metal	Treat- ment	l Min.	30 Mins.	50 Mins.	60 Mins.	24 Hrs.	Ц8 Hrs.
3180 16-A	Zn	Cronak	1,063	1.055	1.048	1.045	qua qua	
-16-c	Zn	Iridite	1.064	1.074	1.075	1.075		
19-A	Çd	Cronak	0.786	0.762	0.737	0.733		Ann 1610
19-c	Cd	Iridite	0.786	0.778	0.776	0.774		est des
—16 - E	Zn	Cronak	1080	1.053	1.053	1.052	1.052	1.069
16-F	Zn	Iridite	1.067	1.051	1.048	1.050	1.062	1.065
19-E	Cd	Cronak	0.788	0.789	0.776	0.770	0.768	0.779
19 - F	Cq	Iridite	0.790	0.787	0.778	0.779	0.774	0.777

^{*} All values are negative.

TABLE 30. INITIAL AND 24-HOUR DYNAMIC POTENTIAL AND CORROSION CURRENT DATA FOR CAST ZINC AND CADMIUM SPECIMENS TREATED BY THE CRONAK OR IRIDITE PROCESSES. THESE SPECIMENS WERE COUPLED WITH STEEL AND IMMERSED IN 3 PER CENT SODIUM CHLORIDE SOLUTION FOR 24 HOURS AT 90°F., SATURATED CALOMEL SCALE

			Initial M	easurements Corrosion	24-Hour k	leasurements Corrosion
Specimen No•	Metal	Treat⇒ ment	Coupled Alloy (Volts)	Current Density (Ma./In.2)	Coupled Alloy (Volts)	Current Density (Ma./In. ²)
3180—16 - B	Zn	Cronak	1.043	0.69	1.055	0.65
16-D	Zn	Iridite	1.034	0.72	1.052	0.55
—19- B	Cđ	Cronak	0.743	0.13	0.729	0•26
19-D	Cq	Iridite	0.758	0.22	0.737	0.25

TABLE 31. BATH COMPOSITIONS AND PLATING DATA FOR ELECTRODEPOSITED ZINC-TIN ALLOYS

Alloy Composition, (Per Cent)	85 Zn- 15 Sn	59 Zn- 41 Sn	37 Zn- 63 Sn	20 Zn- 30 Sn	15 Zn- 05 Sn
Sn (as Ha ₂ SnO ₃) (g./1.)	7.5	30	30	30	30
In [as In(CH)2.](g./1.)	60	25	12	5	3
Total MaCN (g./1.)	197	101	53	32	26
Free MaO H (g./1.)	6	ક	5	6	6
Temperature (°F.)	1.60	160	160	160	160
Current density (Amps./Gq. Ft.)	20	20	20	20	20
Minutes to Plate 0.001 inch	60	52	60	60	60

TARLE 32. BATH COMPOSITIONS AND PLATING DATA FOR ELECTRODEPOSITED CADMINISTS ILVER ALLOYS

Alloy Composition (Per Cont)	94 Cd-6 Ag	97 Cd-3 Ag
Cd/as Cd(CN)2_7(g/1)	28	28
Ag(as Ag CN) (g/1)	1	0.5
Free NaCN	55	55
Total Na2003	5	5
Total NaOH	3.75	3.75
Temporature (°F.)	90	90
Current density (Amps./Sq. Ft.)	15	15
Minutes to plate 0.001 inch	40	45

TABLE 33. POTENTIAL-TIME DATA FOR CAST ZINC-NICKEL ALLOYS, MEASURED AT 90°F., IN 3 PER CENT SODIUM CHLORIDE SOLUTION, DISTILLED WATER, AND DISTILLED WATER SATURATED WITH CARBON DIOXIDE, SATURATED CALOMEL SCALE, VALUES IN VOLTS*

				s at Elap	sed Time		
Specimen		1	30	50	60%×	75	90
No.	Z Ni	Min.	Mins.	Mins.	Mins.	Mins.	Mins.
	(3	Per Cent	Sodium Ch	loride So	lution)		
287583-A-1	0.03	1.032	1.047	1.050	1.050	***	pr
83-B-1	2.58	1.039	1.049	1.051	1.052		****
83-D-1	11.44	1.027	1.048	1.049	1.049	*****	
83-E-1	11.9	1.035	1.051	1.051	1.052		
83-G-1	47.2	0.334	0.398	0.401	0.402	-	*****
		(Di	stilled W	ater)			
2875—83-A-1	0.03				0.770	0.769	0.780
83-B-1	2.58				0.882	0.885	0.90
83-D-1	11.44				0.852	0.807	0.77
83-E-1	11.9				0.870	0.901	0.87
83-G-1	47.2				0.145	0.134	0.12
(Di	stilled W	later Satu	urated Wit	h Carbon	Dioxide)		
287583-A-1	0.03	1.055	1.061	1.060	1.063		
-83-B-1	2.58	1.068	1.093	1.091	1.088		
83-D-1	11.44	1.053	1.073	1.076	1.077		
83-E-1	11.9	1.062	1.072	1.073	1.074		
83-G-1	47.2	0.473	0.501	0.511	0.514		

^{*} All values are negative.

^{*** 60-}minute values plotted in Figure 26.

TABLE 34. POTENTIAL-TIME DATA FOR CAST CADMIUM-NICKEL ALLOYS, MEASURED AT 90°F, IN 3 PERCENT SODIUM CHLORIDE SOLUTION, DISTILLED WATER, AND DISTILLED WATER SATURATED WITH CARBON DIOXIDE, SATURATED CALOMEL SCALE, VALUES IN VOLTS*

		V.	lto at Ela	apsed Time	of:	
% Ni	1 Min.	30 Mins.	50 Mins.	60** Mins.	75 Mins.	90 Mins.
(3 Per Cent	Sodium Ch	iloride So	lution)		
	0.814	0.817	0.816	0.315	•••	0.810
	0.813	0.613	0.616	0.315	-	0.008
	(1)	istilled :	later)			
0.84				0.51.6	0.490	0.474
				0.534	. 0.514	0.488
(Di	atilled Wate	or Saturat	ed With C	urbon Diox	ido)	
0.84	0.723	0.734	0.737	0.737		
2.75	0.712	0.722	0.777	0.729		
	0.84 2.75 0.84 2.75 (Dis	(3 Per Cent 0.84 0.814 2.75 0.813 (1 0.84 2.75 (Distilled Wate 0.84 0.723	1 30 Min. Mins. (3 Per Cent Sedium Ch. 0.84 0.814 0.817 2.75 0.813 0.818 (Distilled Seturation of the Control	1 30 50 Min. Mins. Mins. (3 Per Cent Sedium Chloride Second 0.84 0.814 0.817 0.816 2.75 0.813 0.813 0.816 (Distilled Mater) 0.84 2.75 (Distilled Mater Seturated Mith Company 0.737	1 30 50 60 8 8 60 8 8 60 8 8 60 8 8 60 8 8 60 8 8 60 8 8 60 8 8 60 8 8 60 8 8 60 8 8 60 8 8 8 60 8 8 8 60 8 8 8 60 8 8 8 60 8 8 8 60 8 8 8 60 8 8 8 60 8 8 8 8	Min. Mins. Mins. Mins. Mins. Mins. Mins.

^{*} All values are nogative.** 60-minute values plotted in Figure 27.

TABLE 35. FOTENTIAL-TIME DATA FOR CAST ZINC-LEAD ALLOYS. MEASURED AT 90°F., IN 3 PER CENT SODIUM CHLORIDE SOLUTION, DISTILLED WATER, AND DISTILLED WATER SATURATED WITH CARBON DIOXIDE. SATURATED CALOMEL SCALE, VALUES IN VOLTS.*

Specimen			Vol	ts at Elap	osed Time of	:			
No.	% Pb	l Min.	30 Mins.	50 Mins.	60 Mins**	75 Mins.	90 Mins		
		(3 Per 0	ent Sodium	Chloride	Solution)				
318029-D-1	0.52	1.038	1.049	1.051	1.051	****	1.054		
2875—86-A-1	1.04	1.030	1.045	1.040	1.039	****	1.039		
86-I-1	99.05	0.929	0.848	0.830	0.820	****	0.794		
<u> </u>	(Distilled Water)								
318029-D-1	0.52				0.4852	0.892	0.872		
2875—86-A-1	1.04				0.761	0.788	0.811		
86-I-l	99.05				0.549	0.550	0.553		
	(Dis	tilled Wa	iter Satura	ated With (Carbon Diox	ide)			
318029-D-1	0.52	1.067	1.090	1.089	1.089				
287586-1-1	1.04	1.060	1.071	1.062	1.057	e-main			
86-I-l	99.05	0.575	0.501	0.492	0.489		****		

^{*} All values are negative.

^{** 60-}minute values plotted in Figure 28.

TABLE 36. POTENTIAL-TIME DATA FOR CAST CADMIUM-LEAD ALLOYS, MEASURED AT 90°F., IN 3 PER CENT SCDIUM CHLORIDE SOLUTION, DISTILLED WATER, AND DISTILLED WATER SATURATED WITH CARBON DIOXIDE. SATURATED CALOMEL SCALE, VALUES IN VOLTS.*

Specimen			v	olts at E	Lapsed Time	of:	
No.	% Fd	l Min.	30 Mins.	50 Mins.	60 Mins.	75 Mins.	90 Mins
		(3 Per C	ent Sodium	Chloride	Solution)		
318029 - A-1	2.08	0.808	0.812	0.813	0.812	ena.	0.811
29-B-1	6,22	0.800	0.812	0.811	0.810		0.806
29-C-1	13.1	0.774	0.809	0.808	0.808	47740	tot a
gand ann der gant is belighere the striken and elementary o	**************************************	nere en en estable de la company de la compa	(Distil]	ed Water)	ganan saurin saura saiptas da Main Bi	ren eine <u>ein propriesen</u> errebilieren F	
318029-1-1	2.08				0.364	0.395	0.408
29-B-1	6,22				0.386	0.421	0.436
29 - C-1	13.1				0.400	0.500	0.498
	(Dî	stilled V	later Satu	rated With	Carbon Dic	xide)	
318029-A-1	2,,08	0.717	0.741	0.741	0.742	***	, ***n
29-B-1	6.22	0.714	0.743	0.742	0.743		*****
29-0-1	13.1	0.715	0.746	0.745	0.746		mileratus

^{*} All values are negative.

^{** 60-}minute values plotted in Figure 29.

TABLE 37. POTENTIAL-TIME DATA FOR CAST ZINC-CHROMIUM ALLOYS, MEASURED AT 90°F, IN 3 PERCENT SODIUM CHLORIDE SOLUTION, DISTILLED WATER, AND DISTILLED WATER SATURATED WITH CARBON DIOXIDE, SATURATED CALOMEL SCALE, VALUES IN VOLTS*

			Vol	ts at Elaps	ed Time o	f:	
Specimen No.	5 Cr	l Nin.	30 Hins.	50 liins.	60** Nins.	75 liins.	90 Mins.
		(3 Per C	ent Sodium	Chloride S	Solution)		
318063-A-1	0.43	1.015	1.033	1.034	1.035	<u>ti</u>	1.036
53-B-1	2.04	1.013	1.035	1.035	1.036	-	1.036
63-C-1	5.36	1.020	1.035	1.035	1.035	-	1.036
			(Disti	lled Tater)		
313063-:-1	0.4ပ				0.792	0.030	0.632
63-B-1	2.04				0.738	0.785	0.709
63-C-1	5.36				0.725	0.772	0.304
	(D)	stilled T	ater Satur	ited With	Carbon Dio	cride)	
318063-1	0.40	1.055	1.052	1.055	1.056	***	-
63-B-1	2.04	1.04,3	1.055	1.059	1.061		
63-C-1	5.36	1.047	1.053	1.057	1.053	-	~~

All values are negative.
60-minute values plotted in Figure 30.

TABLE 38. POTENTIAL-TIME DATA FOR CAST ZINC-MANGANESE ALLOYS, MEASURED AT 90°F., IN 3 PER CENT SODIUM CHLORIDE SOLUTION, DISTILLED WATER, AND DISTILLED WATER SATURATED WITH CARBON DIOXIDE. SATURATED CALCAEL SCALE, VALUES IN VOLTS*

Specimen					ed Time of:				
No.	% Mn	l Min.	30 Mins.	50 Mins.	60 Mins.**	75 Mins.	90 Mins.		
		(3	Per Cent S	Sodium Chlo	oride Solutio	n)			
3180—60-A-1	1.65	1.036	1.056	1.058	1.059	direction .	teringua.		
60-B-1	3.04	1.037	1.055	1.057	1.057				
60-C-1	5.18	1.036	1.056	1.057	1.058	GP-MS			
60-D-1	9.60	1.040	1.059	1.060	1.061		~~		
(Distilled Water)									
3180—60-A-1	1.65	****		****	0.869	0.885	0.912		
60-B-1	3.04		~~~		0.844	0.858	0.868		
60-C-1	5,18	~~		***	0.826	0.852	0.852		
60-D-1	9.60	***	****	***	0.845	0.855	0.869		
	(Distille	ed Water S	aturated W	ith Carbon Di	loxide)			
318060-A-1	1.65	1.076	1.063	1.069	1.071	***	-		
60-B-1	3.04	1.065	1.062	1.065	1.066	***			
60-C-1	5.18	1.062	1.060	1.063	1.064	- Charles	1000		
60-D-1	9.60	1.066	1.056	1.059	1,060	***			

^{*} All values are negative.

^{**} Sixty-minute values are plotted in Figure 31.

TABLE 39. POTENTIAL-TIME DATA FOR ELECTRODEPOSITED ZINC-TIN, CADMIUM-SILVER, AND ZINC-LEAD ALLOYS, MEASURED AT 90°F, IN 3 PERCENT SODIUM CHLORIDE SOLUTION, SATURATED CALOMEL SCALE, VALUES IN VOLTS*

3pocimon	ជ Sn	1 Min.	Volts at 30 Nins.	Flapsed Time of: 50 Nins,	60 liins.**
No.	<i>J</i> 3 U11				
			(Zinc-Tin)		
2010 22 1	15	1.0/3	1.067	1.070	1.070
394223-A	-	1.032	1.053	1.058	1.059
22-A	41		1.013	1.022	1.023
16-A	63	1.003	-		0.930
-14-1	80	1.010	0.982	0.974	
—15-A	85	0.953	0.302	0.795	0.779
	♬ Ag		(Cadmium-Silver	•)	,
••	· ·	0.814	0.832	0.824	0.825
3942-20-H			0.826	0.826	. 0.826
-21-E	5.75	0.522	0,020		
	s Pb		(Zinc-Load)		
		7 022	1.050	1.051	1.052
3363-20-	17.7	1.033		1.062	1.062
-21-	B 13.3	1.030	1.060	1.000€	• • • • • • • • • • • • • • • • • • • •

^{*} All values are negative.

** 60-minute values for Zinc-Tin alloys are plotted in Figure 32.

TABLE 40. POTENTIAL-TIME DATA FOR ELECTRODEPOSITED POROUS ZINC AND MANGANESE, HEASURED AT 90°F., IN 3 PER CENT SODIUM CHLORIDE SOLUTION. SATURATED CALOMEL SCALE. VALUES IN VOLTS*

	nagana, i lastinga o propinsional con pica.		Volts at Ela	nsed Time of	•
Specimen No.	Treatment	l Min.	30 Mins.	50 Mins.	60 Mins.
		(Porous	zinc)		
3942—10-A	None	1.049	1.063	1.070	1.073
10-H	Oiled	1.021	1.030	1.029	1.031
10-D	Cronak	1.035	1.041	1.039	1.037
10-J	Iridite	1.035	1.047	1.048	1.048
		(Mang	ganese)		
318048-A	# *	1.317	1.292	1.282	1.279
48B	None	1.389	1.312	1.297	1.292

^{*} All values are negative.

^{**} Thirty-second dip in 5 per cent Na₂Cr₂O₇ solution at room temperature

TABLE 41. INITIAL AND 24-HOUR DYNAMIC POTENTIAL AND CORROSION CURRENT DATA FOR CAST ZINC-NICKEL, CADMIUM-NICKEL, AND ZINC-CHROMIUM ALLOYS COUPLED WITH STEEL. COUPLES IMMERSED IN 3 PERCENT SODIUM CHLORIDE SOLUTION AT 90°F, FOR THE 24-HOUR PERIOD. SATURATED CALOMEL SCALE

		Initial L	easurements Corrosion	24-Hour is	easurements Corrosion
Specimen No.	Zni	Coupled Alloy (Volts)	Current Density (Ha./In. ²)	Coupled Alloy (Volts)	Current Density (Ma./In.2)
		(Zinc-Nicke	el Alloys)		
2875-83-A-1	0.03	1.050	0.75	1.057	0.55
83-B-1	2.58	1.043	0.71	1,056	0.47
83-D-1	11.44	1.043	0.65	0.961	0.38
83-E-1	11.9	1.040	0.54	0.913	0.29
83-G-1	47.2	*	*	*	*
		(Cadmium-Nicl	cel Alloys)		
3180-14-A-1	0.84	0.793	0.23	0.735	0.22
14-B-1	2.75	0.795	0.17	0.718	0.25
		(Zinc-Chrom	ium Alloys)		
	%Cr				
3180-63-A-1	0.48	1.022	0,67	1.044	0.57
63-B-1	2.04	1.029	0.64	1.044	0.55
63-C-1	5.36	1,022	0.64	1,045	0.43

^{*}Alloy was more noble than steel. No dynamic measurements were made.

TABLE 42. INITIAL AND 24-HOUR DYNAMIC POTENTIAL AND CORROSION CURRENT DATA FOR CAST ZINC-LEAD, CADMIUM-LEAD, AND COURLENT DATA FOR CAST ZINC-LEAD, CADMIUM-LEAD, AND COUPLED WITH STEEL. COUPLES ZINC-MANGARESE ALLOYS COUPLED WITH STEEL. COUPLES IMMERSED IN 3 PERCENT SODIUM CHLORIDE SOLUTION AT 90°F, FOR THE 24-HOUR PERIOD. SATURATED CALOMEL SCALE

Specimen	%Pb	Initial Re Coupled Alloy (Volts)	asurements Corrosion Current Density (la./In.2)	Coupled	surements forrosion Current Density (ha./In.2)
No.	702	(Zinc-Les	d Alloys)	7 057	0.55
	0.59	1.052	0.81	1.053	
3180-29-D-1	0.52		0.58	1.050	0.52
2875-86-A-1	1.04	1.037	0.00	*	*
86-I-1	99.05	0.687			
		(Cadmium-	Lead Alloys)		0.23
	- 00	0.788	0.32	0.728	
3180-29-A-1	2.08		0.31	0.727	0.25
29-B-1	6.22	0.789	0.29	0.733	0.22
29-0-1	13.1	0.787			
2260-0		(Zinc-Man	ganese Alloys)		
	Zivin		0.40	1.031	0.68
3180-60-A-1	1.65	1.04	- 00	1.039	0.59
60-B-1	~ 04	1.03		1.02	
	- 20	1.0	39 0.74		0.00
60-C-			40 0.74	1.04	1
to measurements were made.					

^{*}Alloy was more noble than steel. No dynamic measurements were made.

APPENDIX IV

This Appendix contains the Bibliography resulting from the literature survey.

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